

# 8 Surface Processes

## ◆ Mass Exchange

- Volatilization
- Reaeration

## ◆ Momentum Transfer

- Oil spills

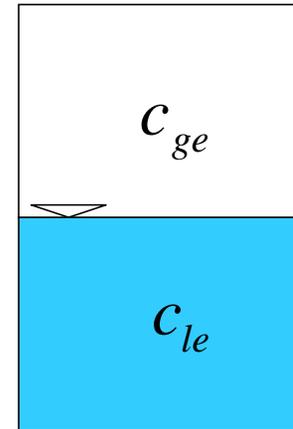
## ◆ Surface Heat Transfer

- Lake temperature models

# Air water exchange

## Equilibrium: Henry's Law

$$H = \frac{c_{ge}}{c_{le}}$$



Typical units for [H]:

atm-m<sup>3</sup>/mol ( $K_H$ ) or dimensionless ( $K_H'$ )

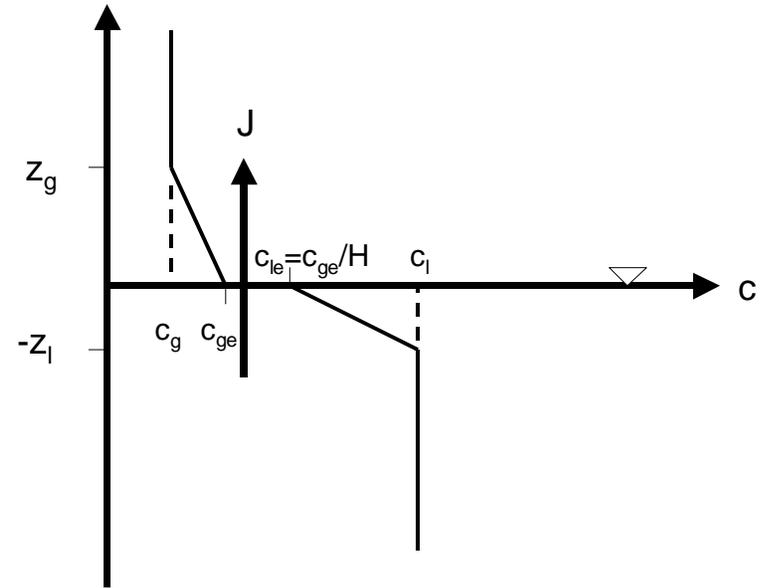
For air  $K_H' \sim 42 K_H$

# Two-film theory

Ex:  
liquid  
side

$$J_l = k_l (c_l - c_{le})$$

$$J_l = D_l \frac{(c_l - c_{le})}{z_l}$$



$$k_l (c_l - c_{le}) = k_g (c_{ge} - c_e) = k (c_l - c_g / H)$$

$$H = \frac{c_{ge}}{c_{le}}$$

3 eqns, 3 unknowns ( $c_{le}$ ,  $c_{ge}$ ,  $k$ )

# Two-film theory

$$\frac{1}{k} = \frac{1}{k_l} + \frac{1}{Hk_g}$$

**1**      **2**

$$c_{ge} - c_g = \frac{k_l(Hc_l - c_g)}{Hk_g + k_l}$$
$$c_l - c_{le} = \frac{k_g(Hc_l - c_g)}{Hk_g + k_l}$$

Resistances in series:

$k_l \ll Hk_g \Rightarrow$  **1** dominates (liquid side controlled)

$k_l \gg Hk_g \Rightarrow$  **2** dominates (gas side controlled)

Medium with lower equilibrium concentration controls

# Typical values for air and water

“Typical” values for air (as gas)

$$D_g \sim 0.1 \text{ cm}^2/\text{s}, \quad 0.1 < z_g < 1 \text{ cm}$$

$$\Rightarrow k_g = D_g/z_g = 0.1 \text{ to } 1 \text{ cm/s}$$

“Typical” values for water (as liquid)

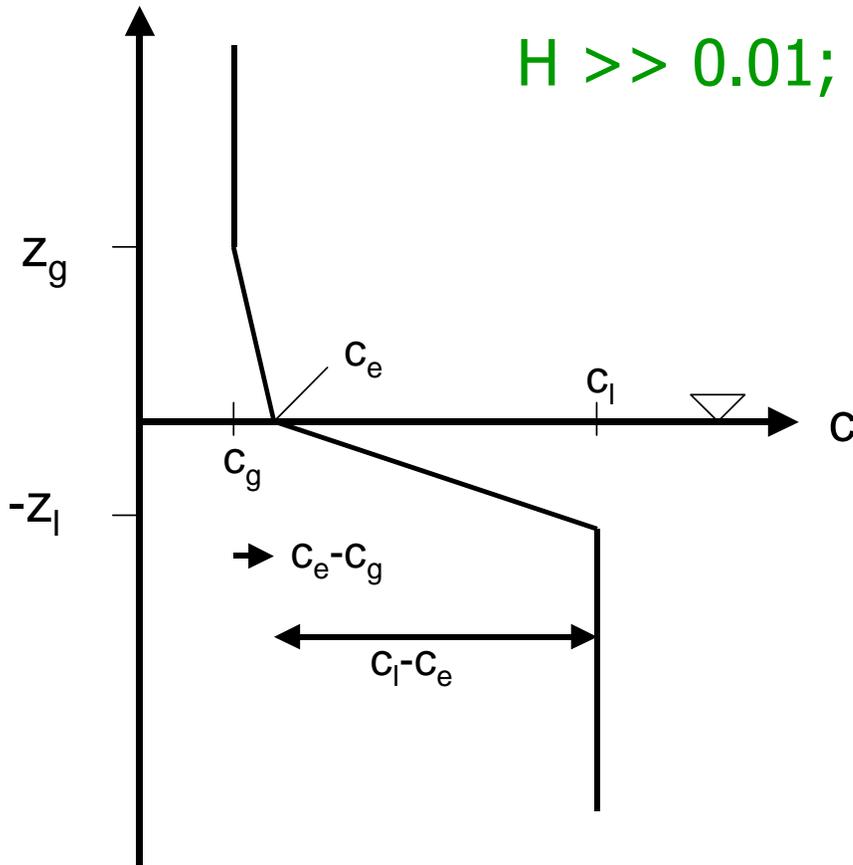
$$D_l \sim 2 \times 10^{-5} \text{ cm}^2/\text{s}, \quad 0.002 < z_l < 0.02 \text{ cm}$$

$$\Rightarrow k_l = D_l/z_l = 10^{-3} \text{ to } 10^{-2} \text{ cm/s}$$

$K_g \sim 100 k_l$  so if  $H \gg 0.01$  then water side controlled (think DO); if  $H \ll 0.01$  then air side controlled (think evaporation)

# Example of liquid side control

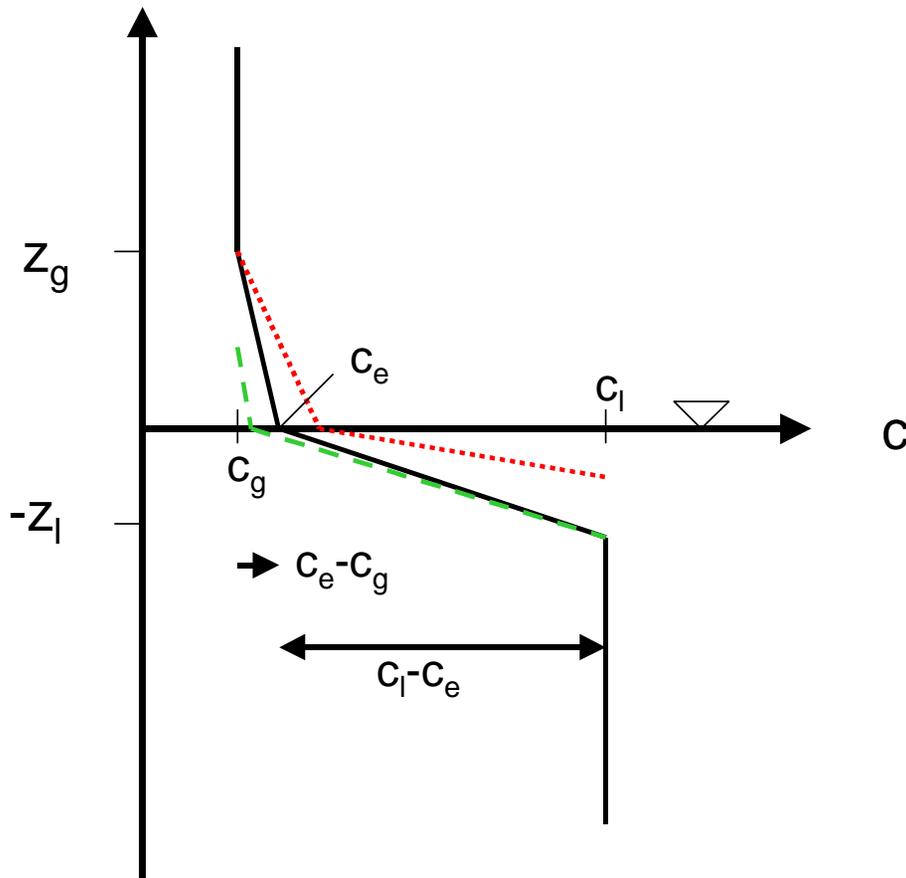
$H \gg 0.01$ ; assume  $H \sim 1 \Rightarrow c_{ge} = c_{le} = c_e$



$$c_e - c_g = \frac{k_l(Hc_l - c_g)}{Hk_g + k_l} \cong (c_l - c_g) \frac{k_l}{k_g}$$

$$c_l - c_e = \frac{k_g(Hc_l - c_g)}{Hk_g + k_l} \cong (c_l - c_g)$$

# Liquid side control, cont'd



If we double  $k_l$  (halve  $z_l$ ),  $(c_e - c_g)$  doubles, both gradients  $\sim$  double  $\Rightarrow$  twice the mass flux; red line

If we double  $k_g$  (halve  $z_g$ ),  $(c_e - c_g)$  is halved, both gradients  $\sim$  const  $\Rightarrow$  similar mass flux; green line

Therefore mass flux controlled by liquid side

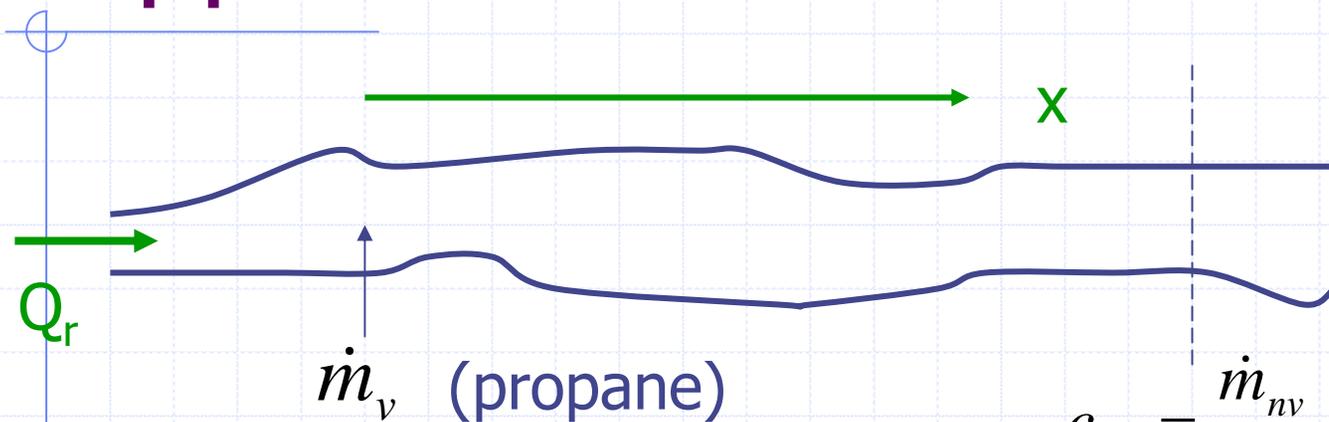
# Surface Renewal Theory

- ◆ Described previously for stream-re-aeration formulae (Chapter 7)
- ◆  $z_1$  (or  $z_w$  or  $\delta$ ) not stagnant, but time-dependent  $\sim [Dt]^{1/2}$ , where  $t$  is reciprocal of a renewal rate, depending on bottom generated turbulence.
- ◆ Thus  $k_1$  (hence  $k$ ) =  $D_1/z_1 \sim D^{1/2}$

# Measurement of gas exchange

- ◆ Gas-evasion experiment: introduce chemically conservative gas (e.g., CO<sub>2</sub>, propane, radon) at  $c > \text{saturation}$ , and watch  $c$  decline with distance due to volatilization
- ◆ In open water bodies (or rivers where you don't know flow rate) introduce a second, non-volatile tracer such as salt.
- ◆ Sometimes use tracer of opportunity

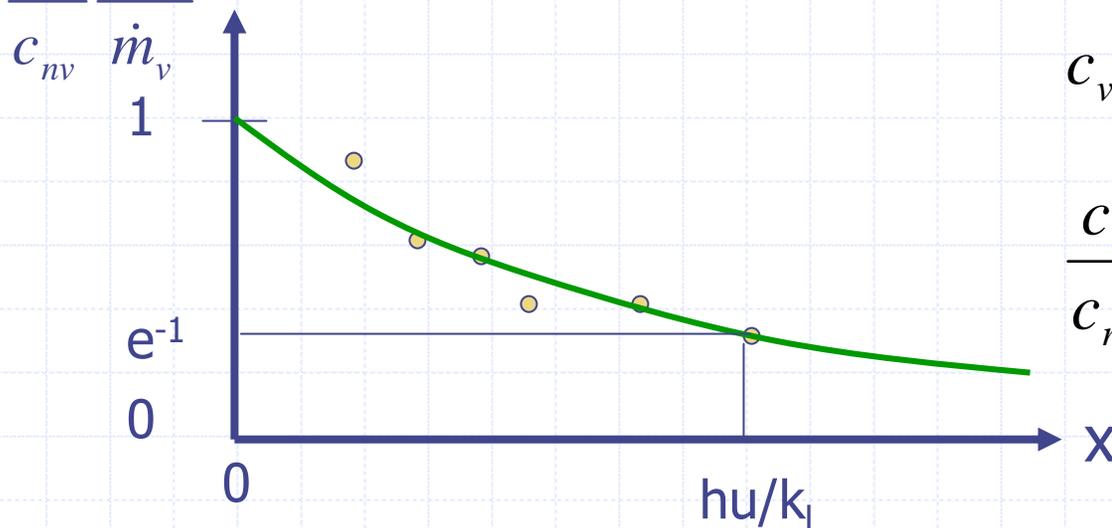
# Application to rivers



$$c_{nv} = \frac{\dot{m}_{nv}}{Q_r}$$

$$\frac{c_v}{c_{nv}} \frac{\dot{m}_{nv}}{\dot{m}_v}$$

$$c_v = \frac{\dot{m}_v}{Q_r} e^{-k_l x / hu}$$



$$\frac{c_v}{c_{nv}} = \frac{\dot{m}_v}{\dot{m}_{nv}} e^{-k_l x / hu}$$

(stream reaeration coefficient  $K_a = k_l/h$ )

# Gasses other than oxygen

- ◆  $K_a \sim D$  (stagnant film),  $D^{1/2}$  (surface renewal),  $D^{2/3}$  (split the difference)
- ◆ From Chapter 1,  $Sc = \nu/D \sim MW^b$  ( $b \sim 0.35$  to  $0.4$ )
- ◆  $K_a/K \sim (D_{O_2}/D)^{2/3} \sim (32/MW)^{-1/4}$
- ◆ Example: Propane  $C_3H_8$ ,  $MW = 44$ 
  - $K_a/K = (32/44)^{-1/4} = 1.08$
  - Calibrations actually shows  $K_a/K \sim 1.39$

# How far downstream must one go?

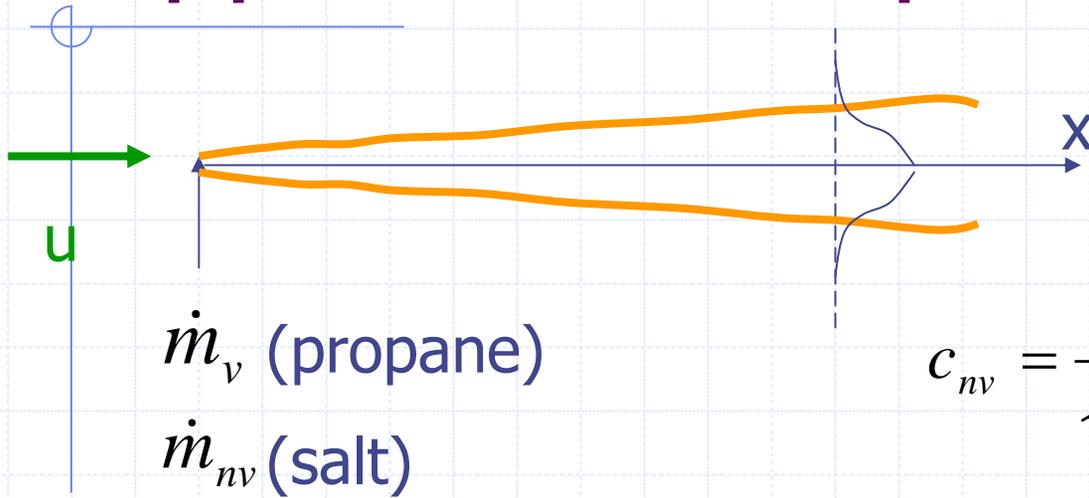
◆ O'Connor-Dobbins at 20°C:

$$K_a = 3.9u^{0.5}/h^{1.5}$$

◆  $u = 0.3 \text{ m/s}$ ,  $h = 1 \text{ m}$ ,  $K_a = 2.1 \text{ d}^{-1}$

◆  $x \sim u/K_a = (0.3 \text{ m/s})(86400\text{s/d})/(2.1\text{d}^{-1})$   
 $\sim 12 \text{ km}$

# Application to open waters

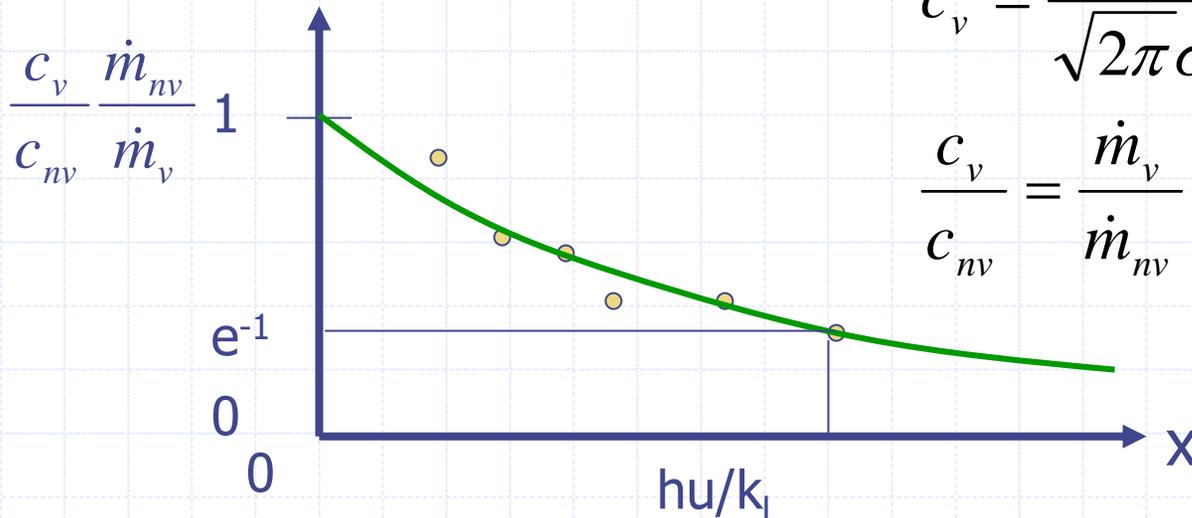


$h$  = water depth or thermocline depth

$$c_{nv} = \frac{\dot{m}_{nv}}{\sqrt{2\pi\sigma u h}} e^{-y^2/2\sigma^2}$$

$$c_v = \frac{\dot{m}_v}{\sqrt{2\pi\sigma u h}} e^{-y^2/2\sigma^2} e^{-k_l x/hu}$$

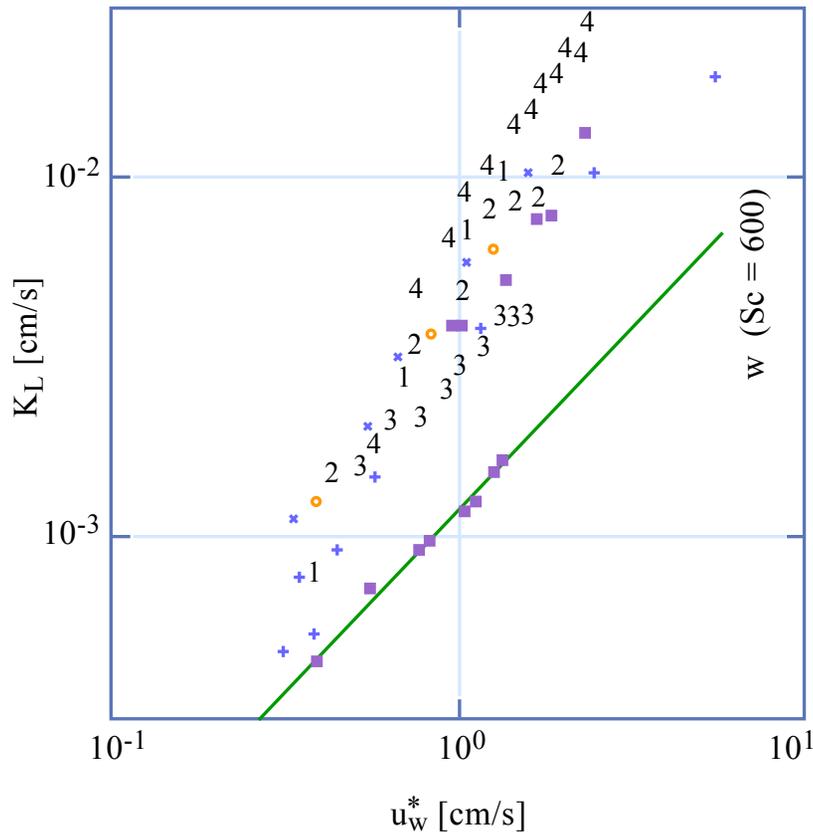
$$\frac{c_v}{c_{nv}} = \frac{\dot{m}_v}{\dot{m}_{nv}} e^{-k_l x/hu}$$



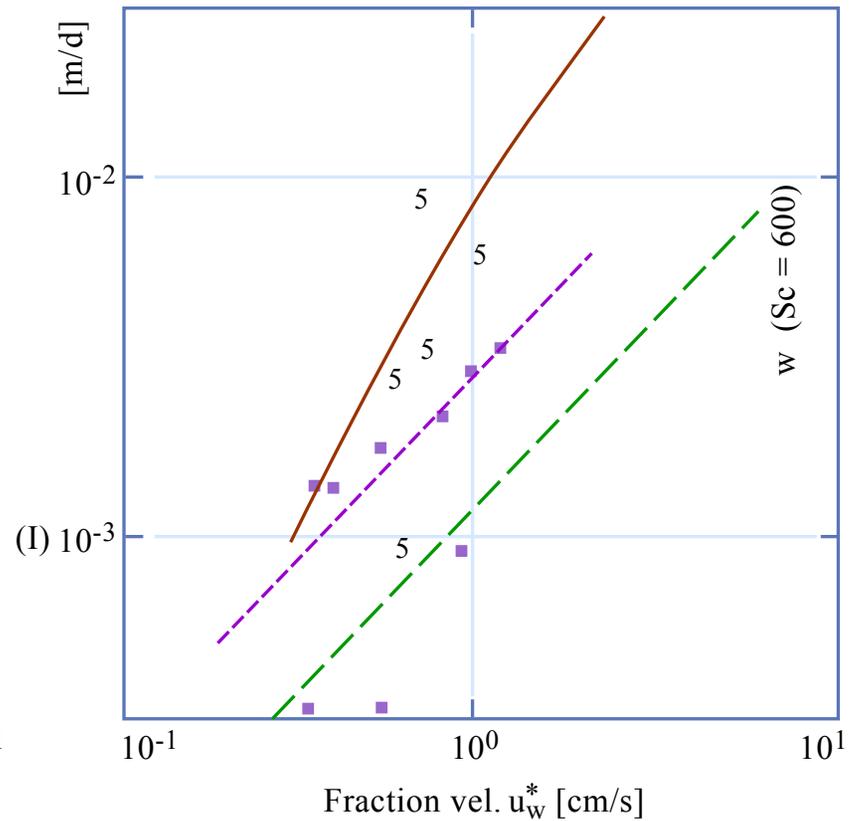
# Mass transfer in lakes and oceans

- ◆ Most contaminants of concern are water side controlled (e.g., DO, VOC)
- ◆ In rivers, source of turbulence is bottom roughness
- ◆ In deep water bodies (lakes, oceans) it is wind stress  $\Rightarrow u_{w*}$  (water-side friction velocity) which affects  $z_l$
- ◆ Contaminants that are air side controlled also affected by wind (through  $z_g$ )

# $k_L$ vs $u_{w*}$



lab

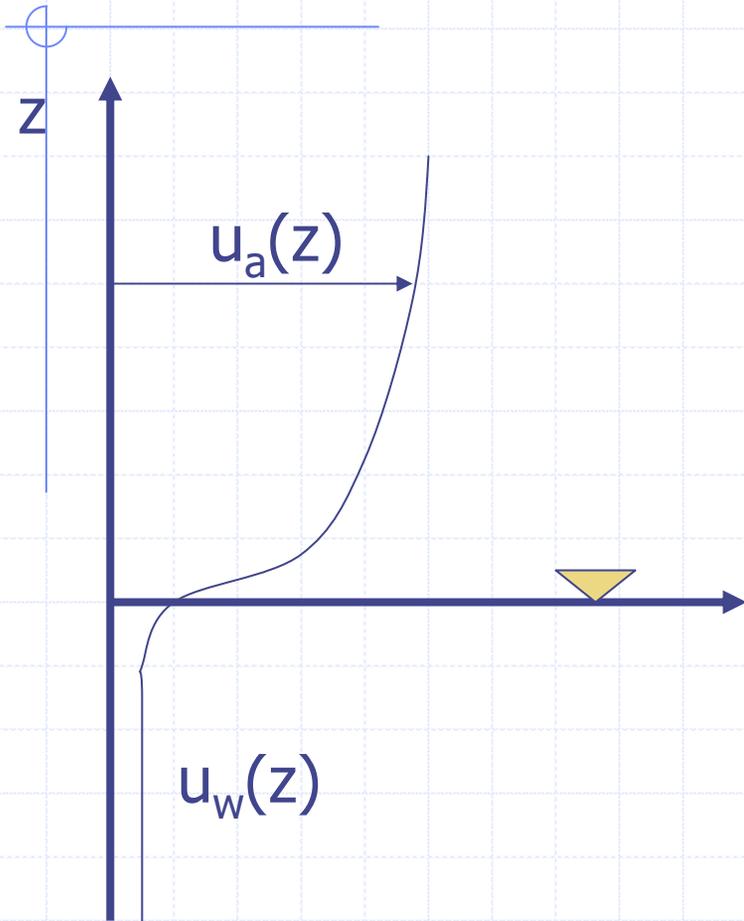


field

Figure by MIT OCW.

$u_{w*}$  because transfer is water side controlled and  $u_{w*}$  is indicator of turbulence; yet  $u_{w*}$  not easily measured

# Wind Stress



$$\tau = C_{10} \rho_a u_{10}^2 = \rho_w u_{w*}^2$$

$$u_{w*} = \sqrt{\frac{C_{10} \rho_a}{\rho_w}} u_{10}$$

$u_{10}$  = 10 m wind speed;

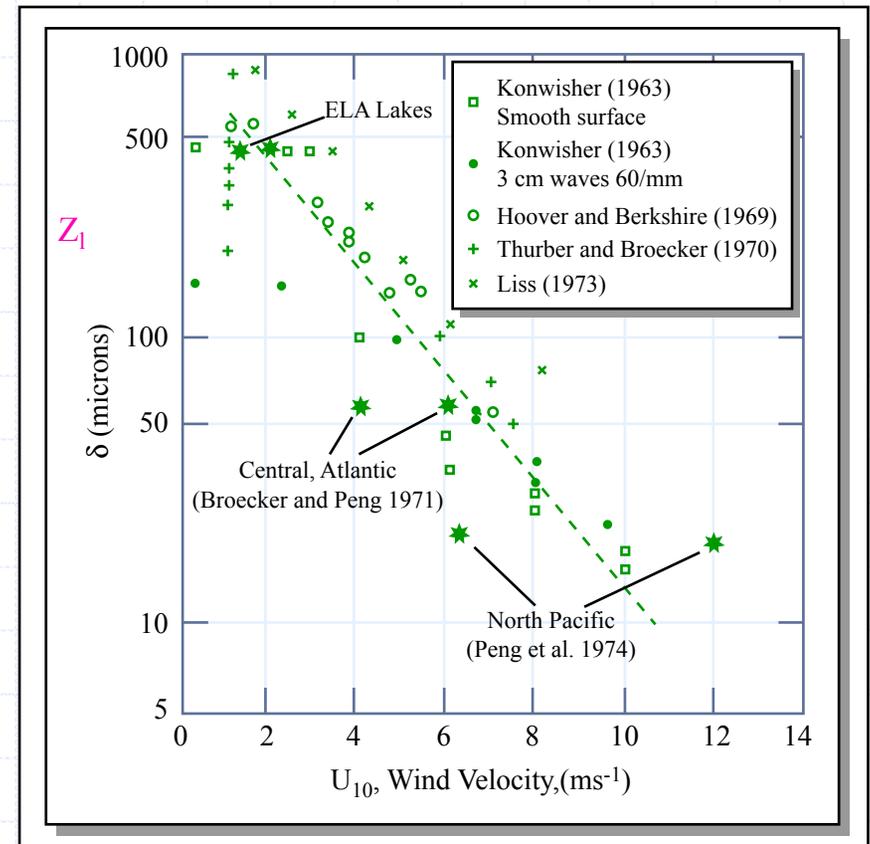
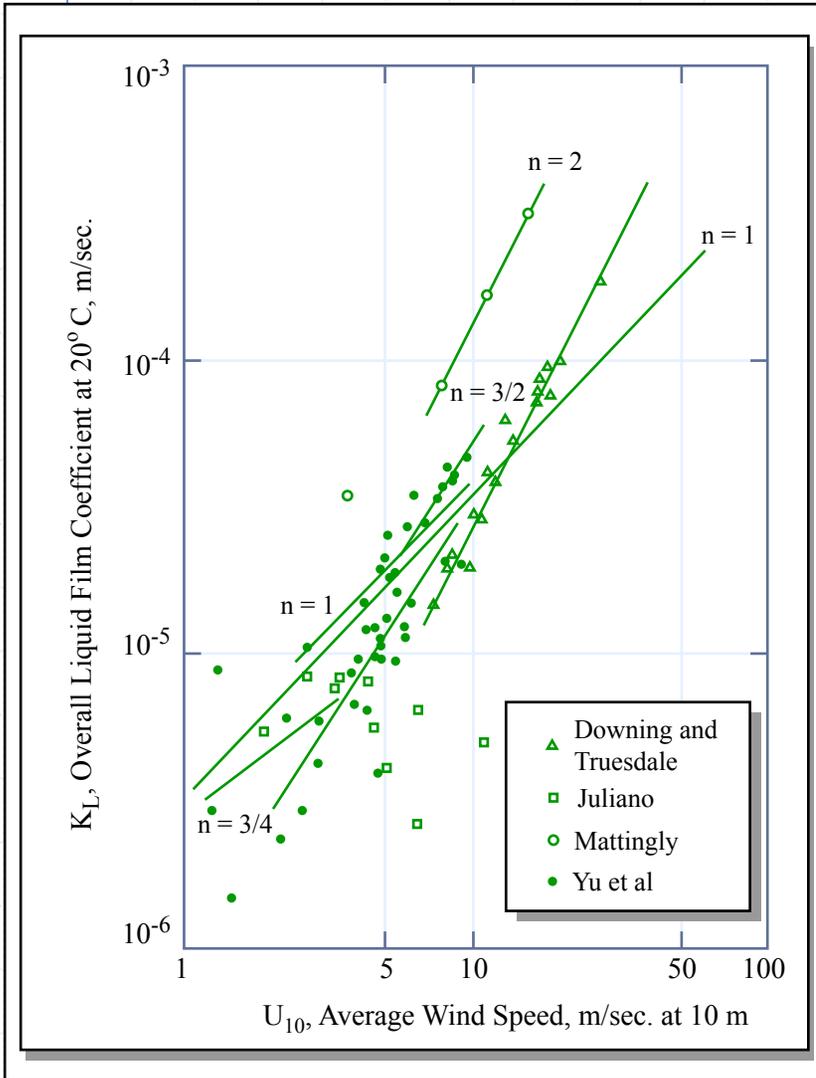
$C_{10}$  = drag coef.

$$C_{10} = (0.8 + 0.065 u_{10}) \times 10^{-3}$$

[ $u_{10} > 1$  m/s; Wu, 1980]

$$u_{10} \rightarrow C_{10} \rightarrow u_{w*} \rightarrow k_1$$

# $k_L$ (or $z_L$ ) vs $U_{10}$



Yu and Hamrick (1984)

Figures by MIT OCW.

Emerson (1075)

# Example film coefficients

$$k_l = 0.0004 + 0.00004u_{10}^2$$

$$k_g = 0.3 + 0.2u_{10}$$

$k_l$  and  $k_g$  in cm/s;  $u_{10}$  in m/s [Schwarzenbach et al, 1993]

Note that both depend on  $u_{10}$

# Examples

Above eqns:

$$u_{10} = 5 \text{ m/s} \Rightarrow k_l = 1.4 \times 10^{-3} \text{ cm/s (green dot);}$$

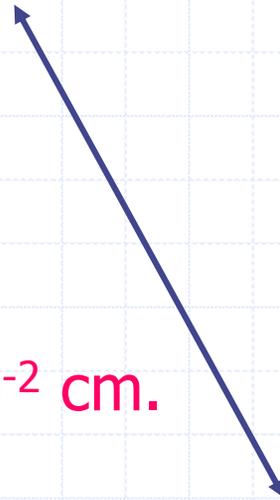
$$k_g = 1.3 \text{ cm/s}$$

Figure 8.8:

$$z_l = \delta = 120 \text{ } \mu\text{m} = 1.2 \times 10^{-2} \text{ cm.}$$

$$\text{For DO, } D = 2 \times 10^{-5} \text{ cm}^2/\text{s}$$

$$k_l = D/z_l = 2 \times 10^{-5} / 1.2 \times 10^{-2} = 1.7 \times 10^{-3} \text{ cm/s (red dot)}$$



# $k_L$ (or $z_L$ ) vs $U_{10}$

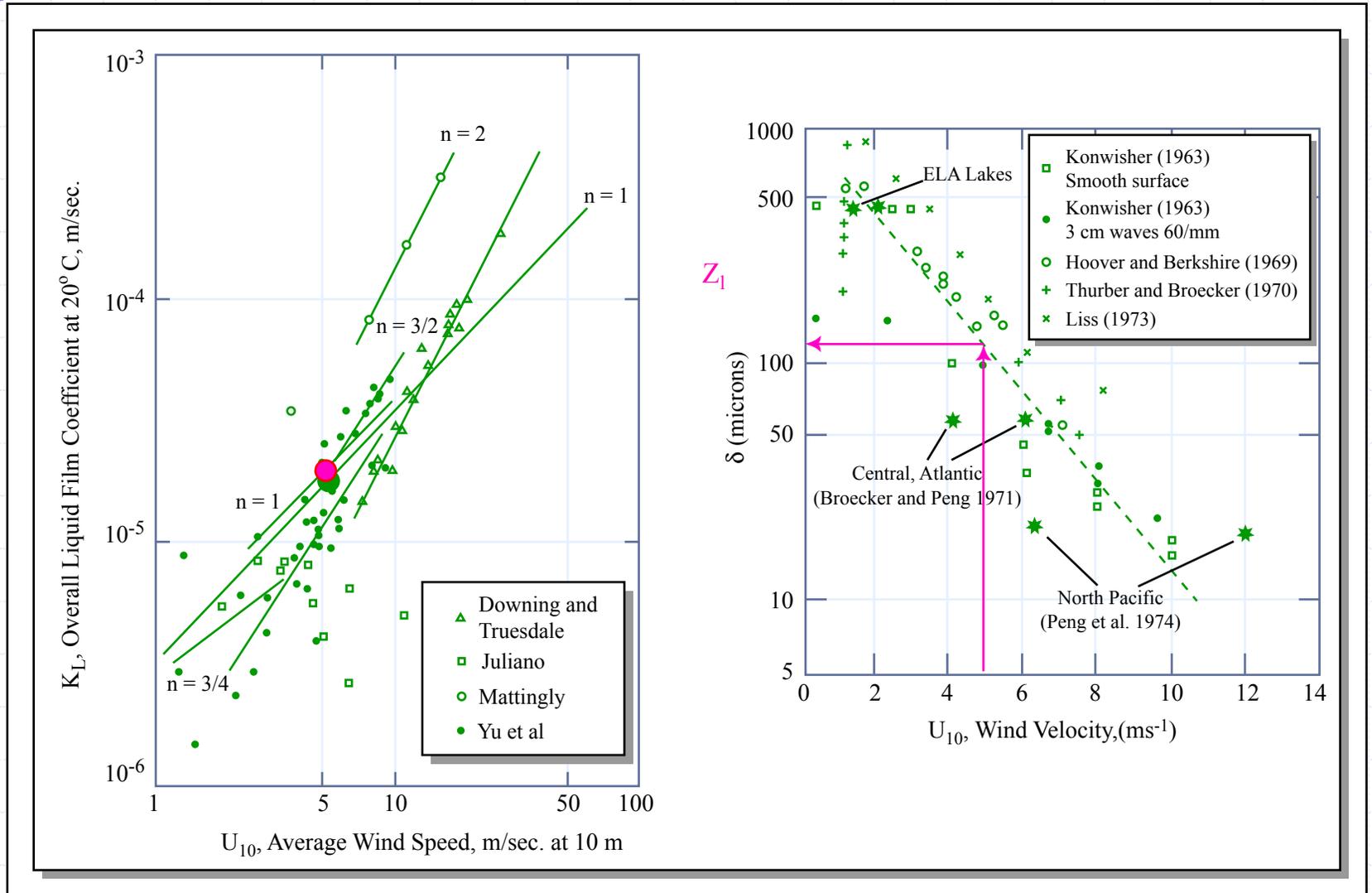


Figure by MIT OCW.

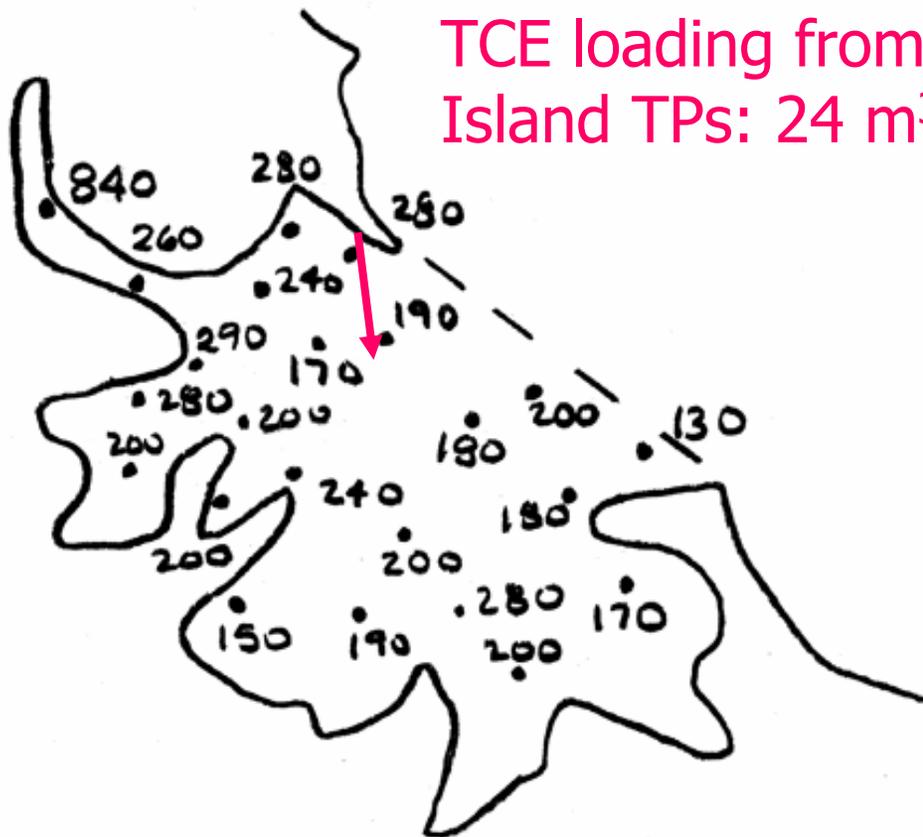
Emerson (1075)

Yu and Hamrick (1984)

# Volatile Halogenated Organic Compound (VHOC) Experiment

- ◆  $\text{CH}_3\text{Cl}_3$  and other one carbon VOCs (THMs) and two carbon VOCs (solvents) discharged with waste water.
- ◆ Used to
  - compute volatilization (assuming known residence time) or
  - compute residence time (with known volatilization)

# TCE data in Boston Harbor



TCE loading from Deer & Nut  
Island TPs:  $24 \text{ m}^3/\text{s}$  at  $11 \mu\text{g}/\text{L}$

Ave harbor TCE  
concentration

$241 \text{ ng}/\text{L}$  (all pts)

$214 \text{ ng}/\text{L}$  (excl. 840)

Harbor volume =  
 $6 \times 10^8 \text{ m}^3$

# TCE Experiment, cont'd

Nominal residence time (w/o volatilization;  
excluding presumed outlier)

$$\tau^* = \frac{\bar{c}V}{Q_o c_o} = \frac{(214 \times 10^{-9} \text{ kg} / \text{m}^3)(6 \times 10^8 \text{ m}^3)}{(24 \text{ m}^3 / \text{s})(86400 \text{ s} / \text{d})(11 \times 10^{-6} \text{ kg} / \text{m}^3)} = 5.6 \text{ d}$$

# TCE Experiment, cont'd

With volatilization

$$V \frac{dc}{dt} = -kAc - Q_f c$$

$$\frac{dc}{dt} = - \underbrace{\left( \frac{kA}{V} + \frac{Q}{V} \right)}_{\kappa^*} c$$

$$\kappa^* = 1/\tau^*$$

$k$  = piston velocity  $\sim k_1$  (water side control)

$\kappa^*$  = bulk removal rate ( $t^{-1}$ )

$V/Q = \tau$  = hydraulic res time

$kA/V = k/h$

For  $\text{CH}_3\text{Cl}_3$   $H = 1.13$  (dimensionless)  $\gg 1 \Rightarrow$  ws control

$D = 1.0 \times 10^{-5} \text{ cm}^2/\text{s}$

# TCE Experiment, cont'd

From Figure 8.8 and  $u_{10} = 5 \text{ m/s}$ ,  $\delta = 1.2 \times 10^{-2} \text{ cm}$

$$k = D/\delta = (1.0 \times 10^{-5}) / (1.2 \times 10^{-2}) = 0.00083 \text{ cm/s} = 3 \text{ cm/hr} = 0.72 \text{ m/d}$$

$$1/t^* = 1/t + k/h$$

$$1/t = 1/t^* - k/h = (1/5.6\text{d}) - (0.72 \text{ m/d})/6\text{m} \\ = 0.18 - 0.12 = 0.06\text{d}^{-1} \Rightarrow \tau = 17 \text{ d}$$

Estimated  $\tau$  is too high; reason is likely extraneous or under-accounted sources of  $\text{CH}_3\text{Cl}_3$

# Momentum Exchange

- ◆ Chapters 2, 3 discussed surface shear stress for eddy diffusivity and hydrodynamic modeling
- ◆ Previous section discussed stress as source of turbulence governing mass exchange
- ◆ Also of interest in transporting floating material, specifically spilled hydrocarbons

# Oil Spills

- ◆ Composition
- ◆ Fate
- ◆ Transport (spreading, advection)
- ◆ Clean-up



# Marine Sources ( $10^3$ MT/yr)

	N. America	Global
Natural Seeps	160	600
Petroleum Extraction	3	38
Petroleum Transport	9	150
Petroleum Consumption	84	480
Total	260	1300

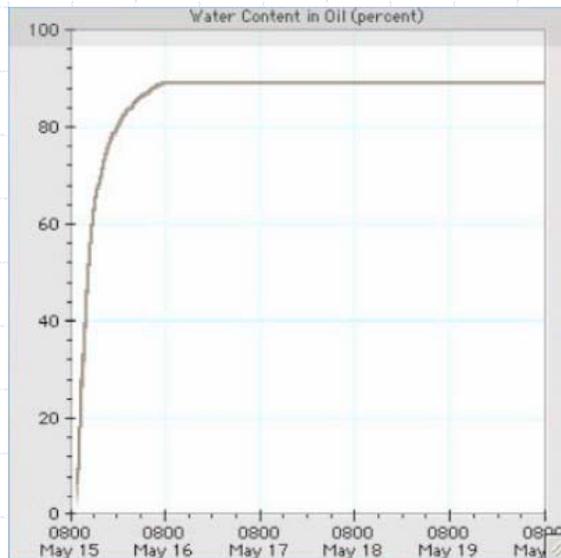
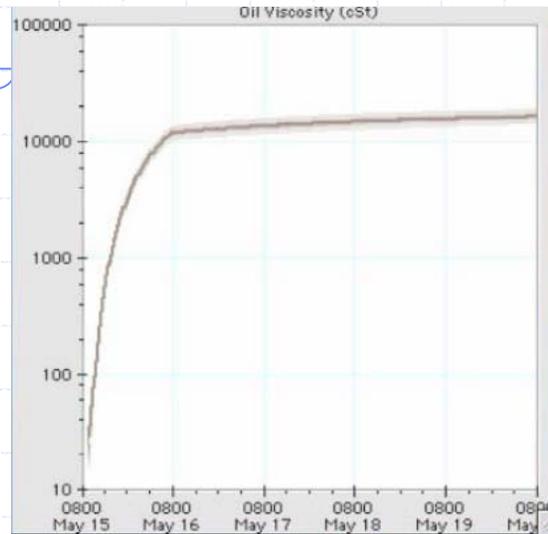
About half is anthropogenic

(Oil in the Sea III, NRC, 2003)

# Composition

- ◆ Crude and Refined Oils
- ◆ Always multiple constituents
- ◆ Characterized by Boiling Point (or distillation cut)

# Fate



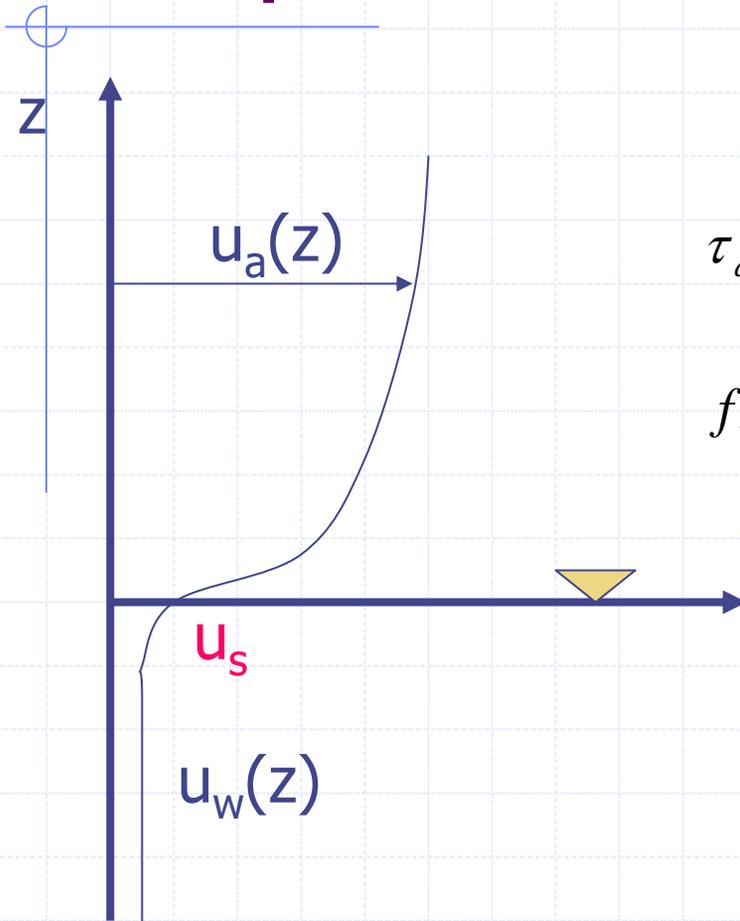
- ◆ Volatilization (lighter fractions)
- ◆ Emulsification (depending on oil)
- ◆ Natural dispersion (if enough energy)
- ◆ Biodegradation
- ◆ Dissolution
- ◆ Photo-oxidation
- ◆ Sediment particle interaction

Output from NOAA's ADIOIS model; independent of transport

# Transport Models

- ◆ Spreading and Advection
- ◆ Pre-planning (evaluate risk)
- ◆ Real-time (assist clean-up; needs to be quick and dirty)
- ◆ Hind-cast (who is responsible, damage assessment)

# Simple advection model



$$\tau_a = \frac{f_a}{2} \rho_a u_a^2 = \frac{f_w}{2} \rho_w (u_s - \bar{u}_w)^2 = \frac{f_w}{2} \rho_w (\Delta u_s)^2$$

$$f_w \cong f_a \rightarrow \frac{\Delta u_s}{u_a} = \sqrt{\frac{\rho_a}{\rho_w}} \cong 0.03$$

Surface current speed  $\sim 3\%$  of wind speed. (Also explained by Stokes Drift due to surface waves)

In which direction?

# Ekman Model

Linearized equations of motion; constant viscosity

$$\frac{\partial u}{\partial t} - \Omega v = E \frac{\partial^2 u}{\partial z^2}$$

$$\Omega = 2\omega \sin \phi \quad \text{Coriolis parameter}$$

$$\frac{\partial v}{\partial t} + \Omega u = E \frac{\partial^2 v}{\partial z^2}$$

$$w = u + iv \quad \text{Complex velocity}$$

$$w = 0$$

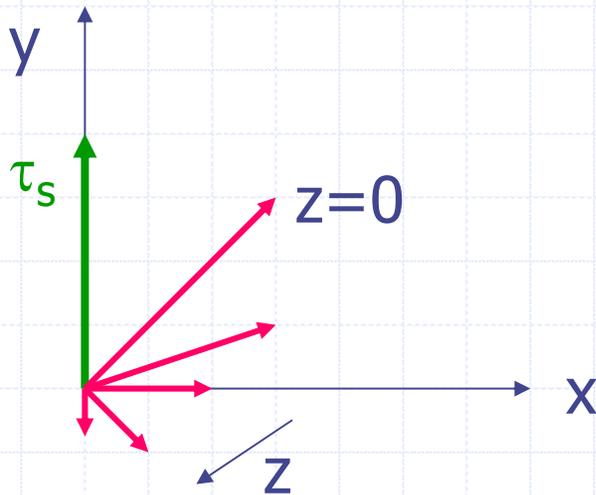
At depth ( $z = -\infty$ )

$$E \frac{\partial w}{\partial z} = \frac{\tau_{sx} + i\tau_{sy}}{\rho_w}$$

At surface ( $z = 0$ )

# Ekman Model, cont'd

$$w = \frac{\tau_{sy}}{\rho_w \sqrt{E\Omega}} \exp\left\{ \sqrt{\frac{\Omega}{2E}} (1+i)z + \frac{i\pi}{4} \right\}$$

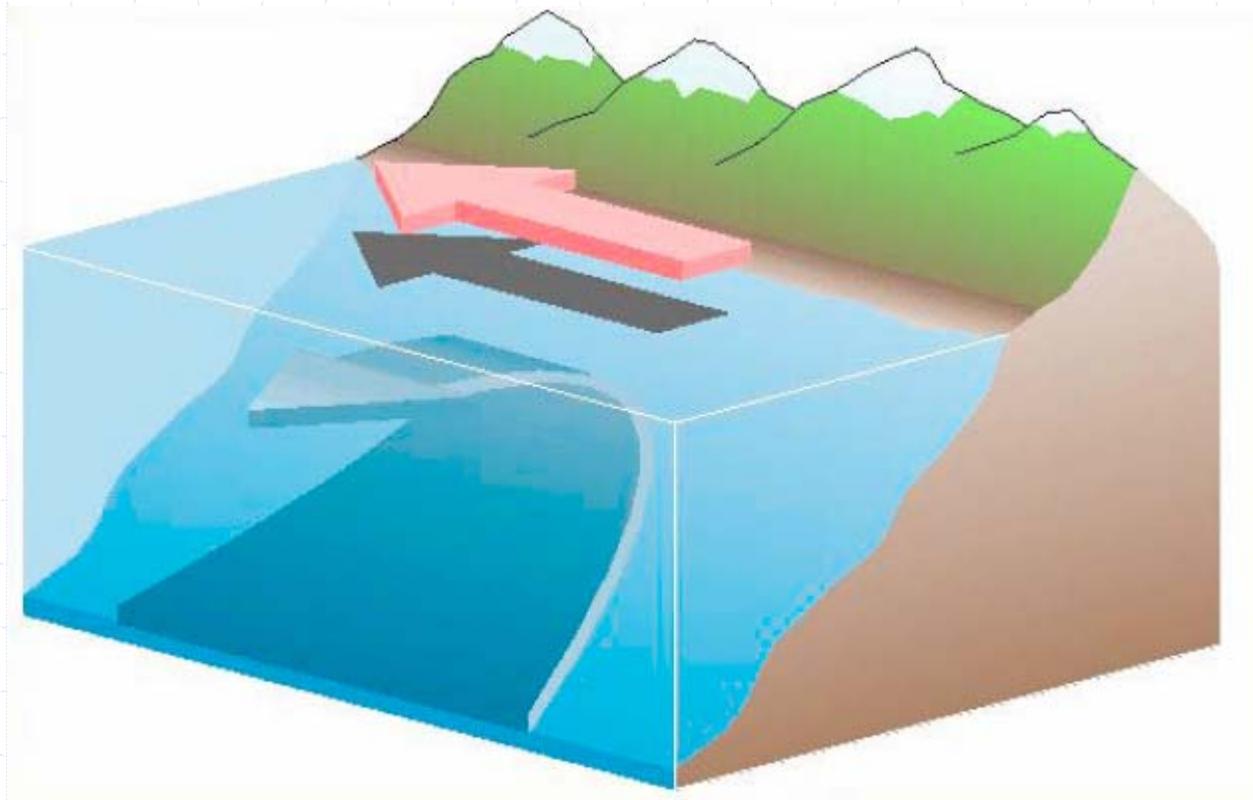


Surface drift 45° to right;

Depth average drift 90° to right

Field experiments show surface drift  $\sim 10^\circ$  to right. Explained by variable vertical viscosity  $E \sim z$  (Madsen, 1977)

# Other effects of wind: Coastal Upwelling/Downwelling



# Other effects of wind: Langmuir Circulation

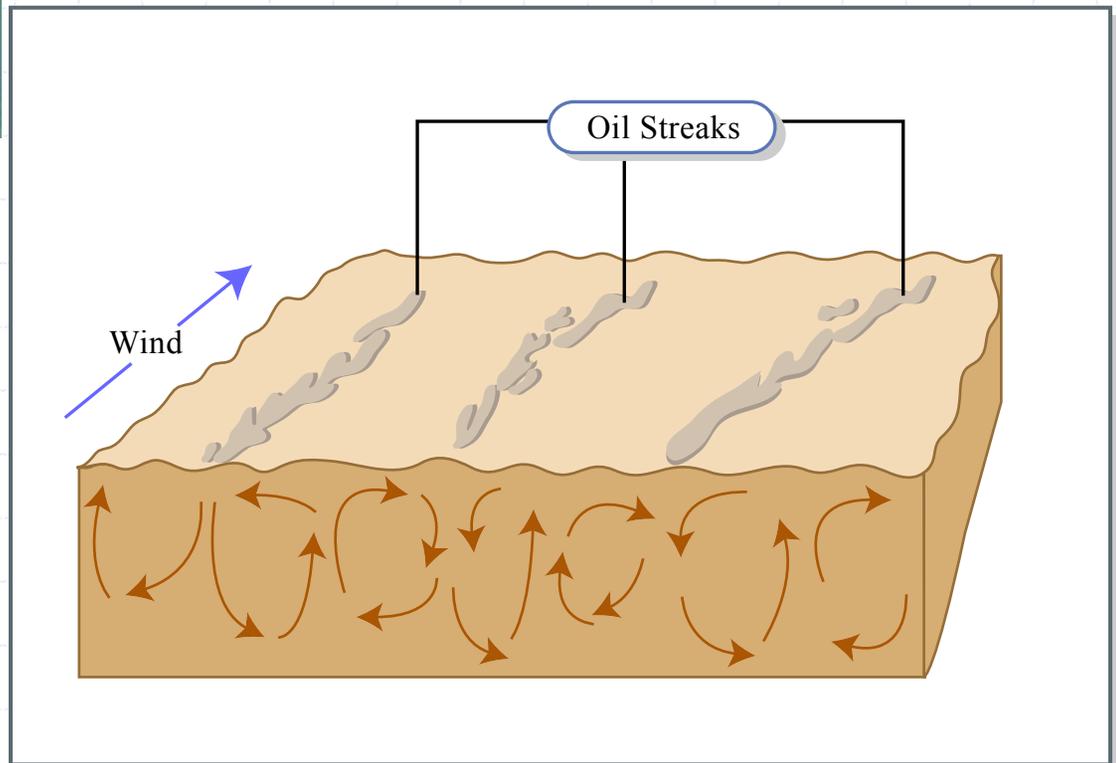
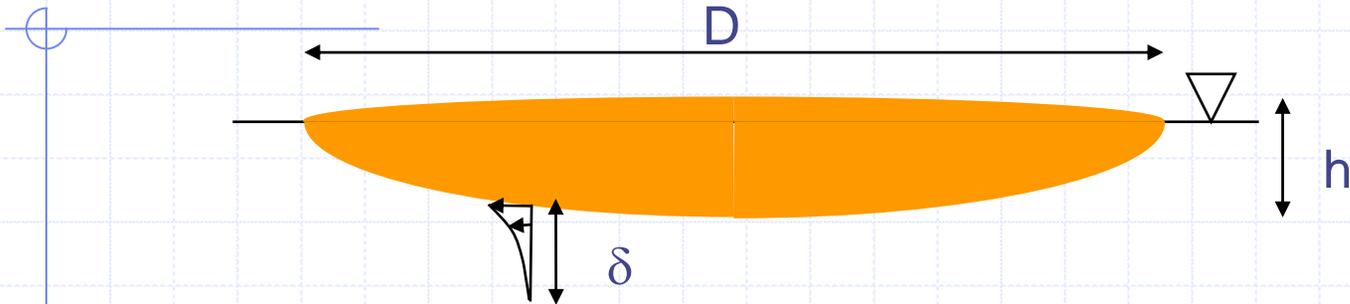


Figure by MIT OCW.

# Idealized Spreading (Fay, 1969)



$$\frac{dD}{dt} \sim \sqrt{g'h} \sim \frac{1}{D} \sqrt{g'V}$$

Gravity-Inertia

$$\frac{dD}{dt} \sim \frac{g'V^2}{D^5} \sqrt{\frac{t}{\nu_w}}$$

Gravity-Viscous

$$\frac{dD}{dt} \sim \frac{f_r}{\rho_w D} \sqrt{\frac{t}{\nu_w}}$$

Surface Tension-Viscous

# Idealized spreading, cont'd

Regime		
Gravity-Inertia	$D = 2k_1[gVt^2]^{1/4}$	$K_1=1.14$
Gravity-Viscous	$D = 2k_2[gV^2t^{3/2}/v_w^{1/2}]^{1/6}$	$K_2=0.98$ to 1.45
Surface Tension-Viscous	$D=2k_3[f_r t^3/\rho_w 2v_w]^{1/4}$	$K_3=1.6$

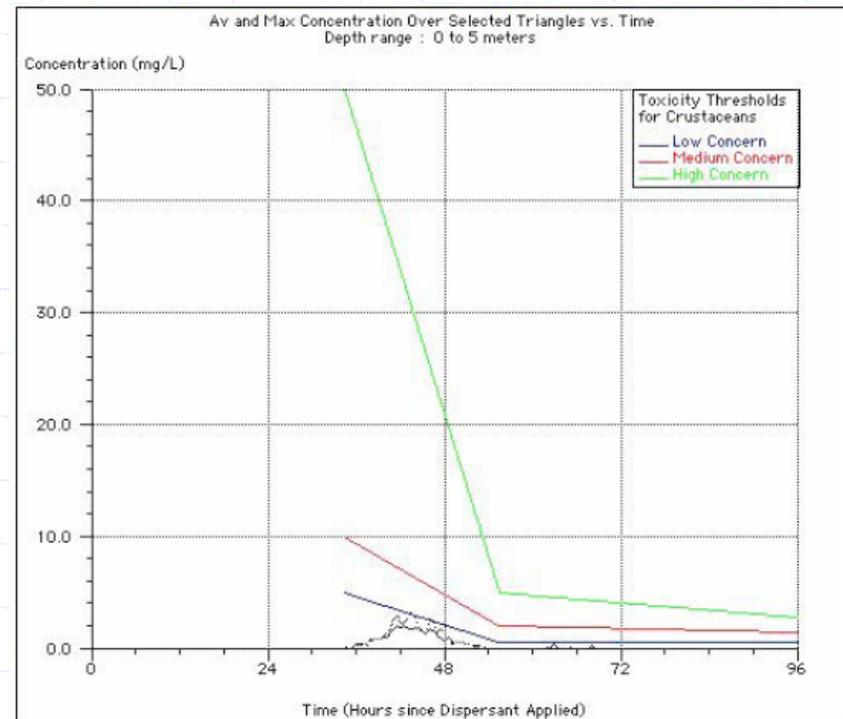
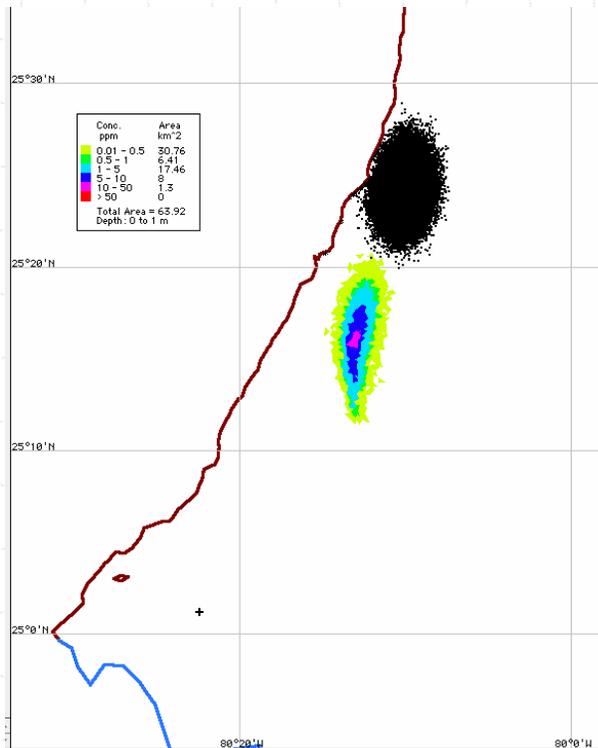
# Comments

- ◆ Theory applies down to slick thickness of about 0.1 mm
- ◆ Additional spreading due to
  - Time-varying spillage
  - Wind, waves and non-uniform currents
  - Dispersion of submerged (slower moving) oil droplets
- ◆ Field experiments show oil often very non-uniform (90% of volume in 10% of area)

# Oil Transport Models

- ◆ Slick advected with underlying surface current plus 3% of wind speed ( $\sim 10\%$  deflection to right)
- ◆ (3-D) models simulate transport of sub-surface dispersed oil.
- ◆ Currents can be observed or predicted (sophistication depends on application—available time)
- ◆ Fate processes often computed independently from transport

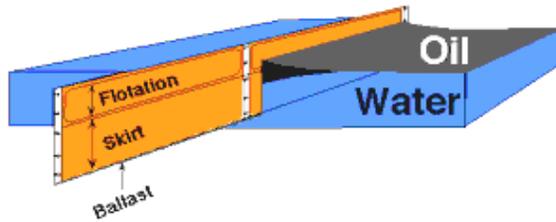
# Model Simulations



NOAA's 3D GNOME; ANS Crude off Coast of Florida

# Mechanical Clean-up

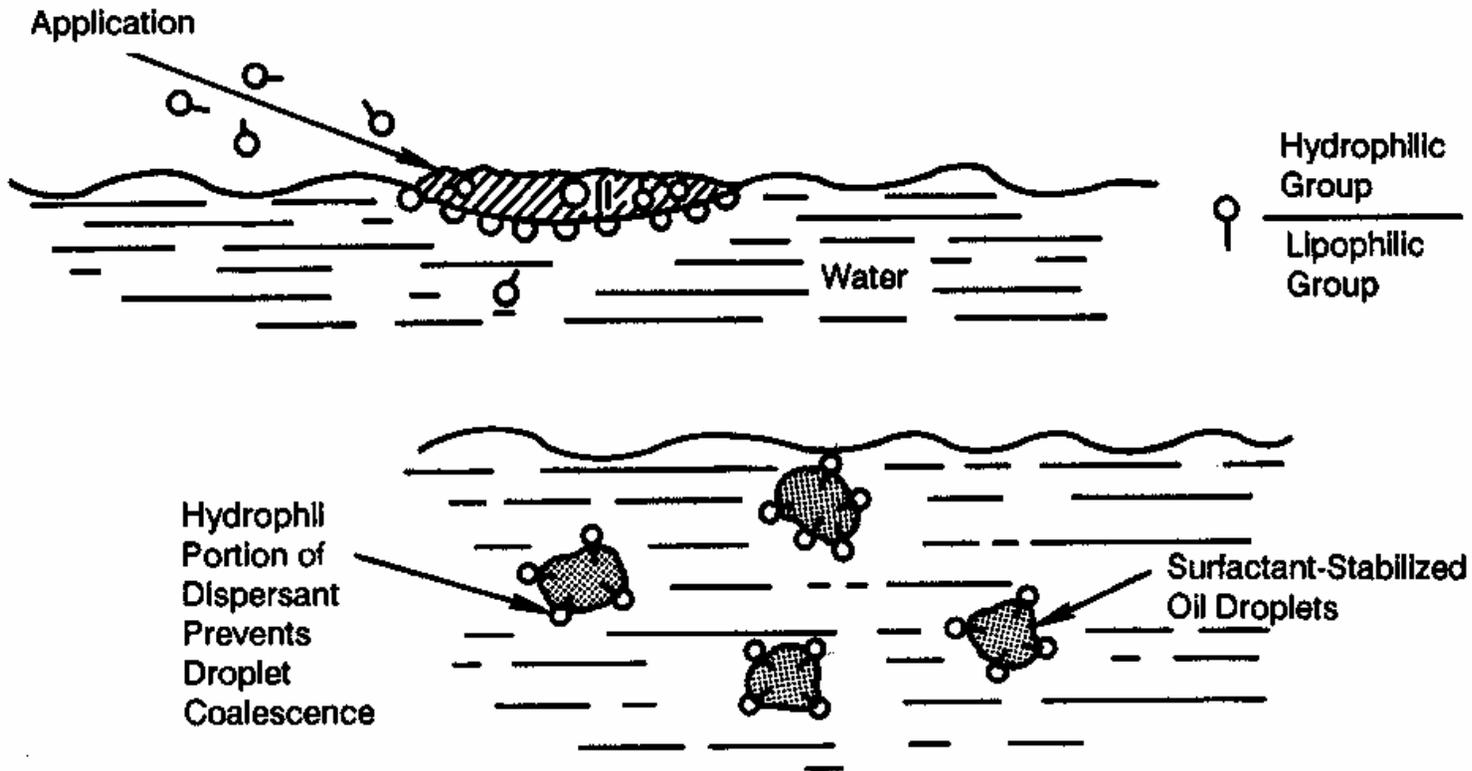
## Oil Containment Boom



# Chemical Dispersion

- ◆ Surfactants that reduce interfacial tension
- ◆ Create dispersed droplets
- ◆ Subsurface/bottom impacts vs surface/shoreline
- ◆ Air (large spills) or boat application
- ◆ Window of opportunity

# Chemical Dispersion, cont'd



# In situ Burning

- ◆ Considered secondary option (like chemical dispersants)
- ◆ Most appropriate for offshore spills (reduced AQ impacts)



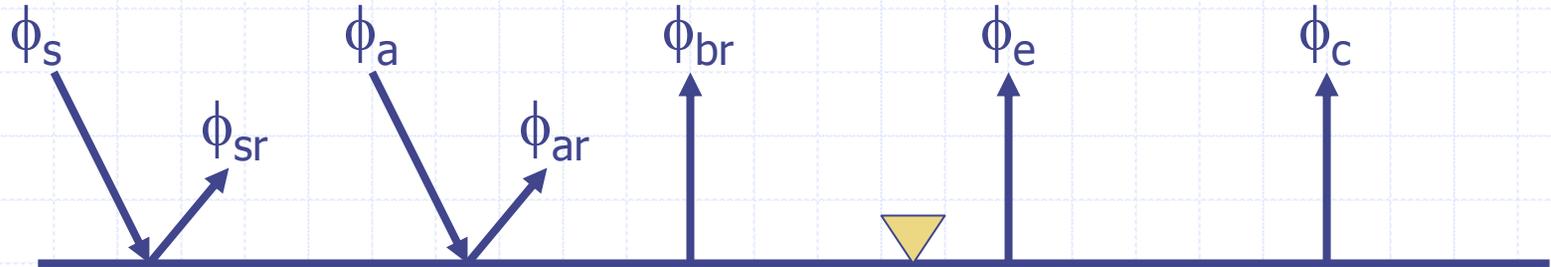
# Surface Heat Transfer and Temperature Modeling

- ◆ Surface heat fluxes
- ◆ Linearized surface heat transfer
- ◆ Cooling ponds
- ◆ Natural lakes and reservoirs

# Importance of Temperature

- ◆ Important WQ parameter
  - Thermal pollution
  - Species preference (fish habitat)
- ◆ Affects rate constants
  - $K = K_{20} \theta^{T-20}$
- ◆ Produces density stratification
  - $\rho = \rho(T)$
- ◆ Important tracer (e.g.,  $E_z$ )

# Surface Heat Transfer ( $\text{W}\cdot\text{m}^{-2}$ )



Net solar, $\phi_{sn}$	60 to 300
Net atmospheric, $\phi_{an}$	200 to 450
Back radiation, $\phi_r$	250 to 500
Evaporation, $\phi_e$	0 to 350
"Conduction", $\phi_c$	-70 to 200

$$\phi_n = \phi_{sn} + \phi_{an} - \phi_{br} - \phi_e - \phi_c$$

# Solar Radiation

- ◆ Short wave length ( $< 3\mu\text{m}$ )
- ◆ Direct plus diffuse (scattered, reflected)
- ◆ Absorbed & re-radiated ( $> 3\mu\text{m}$ ) by clouds
- ◆ Measured by pyranometer
- ◆ Incident clear sky radiation calculated from latitude, date and time of day
- ◆ Corrections for cloud cover and reflection

# Net Solar Radiation (cont'd)

$\phi_{sr}/\phi_s$ (%)	Jan	Feb	Mar	Apr	May	Jun	Jul	Aug	Sep	Oct	Nov	Dec
	9	7	7	6	6	6	6	6	6	7	9	10

$$\phi_{sn} = \phi_s - \phi_{sr} \cong 0.94\phi_{sc} (1 - 0.65C^2)$$

C = fractional cloud cover

# Depth-variation of solar radiation

- ◆ Measured with Secchi disk or *in-situ* pyranometer

$$\phi_z = (1 - \beta)\phi_{sn}e^{-\eta z}$$

$$\eta = \frac{1.7}{d_D}$$

$$\beta \sim 0.5$$



# Atmospheric Radiation

- ◆ Long wave length ( $> 3\mu\text{m}$ )
- ◆ Re-radiated from atmosphere
- ◆ Measured by pyrgeometer
- ◆ Incident clear sky radiation calculated from absolute air temperature, vapor pressure
- ◆ Corrections for cloud cover and reflection

# Incident Radiation Formulae

$$\phi_{ac} = \varepsilon \sigma (T_a + 273)^4$$

$\sigma$  = Stefan-Boltzman const ( $5.7 \times 10^{-8}$  W/m<sup>2</sup>-°K<sup>4</sup>)

$\varepsilon$  = emissivity (dimensionless)

$$\varepsilon = 0.92 \times 10^{-5} (T_a + 273)^2 \quad \text{Swinbank (1963)}$$

$$\varepsilon = \left\{ 1.0 - 0.26 / \exp[7.77 \times 10^{-5} (T_a)^2] \right\} \quad \text{Itso-Jackson (1969)}$$

$$\varepsilon = 1.24 \left( \frac{e}{(T_a + 273)} \right)^{1/7}$$

$e$  = vapor pressure, mbar

Brutsaert (1975)

# Net Atmospheric radiation

$$\phi_{an} = 0.97 \varepsilon \sigma (T_a + 273)^4 (1.0 + 0.17 C^2)$$

C = fractional cloud cover

~3% reflection

# Back Radiation

- ◆ Water surface is nearly a black body
  - ( $\varepsilon \sim 0.97$ )

$$\phi_{br} = 0.97 \sigma (T_s + 273)^4 = 5.5 \times 10^{-8} (T_s + 273)^4$$

# Evaporative Heat Flux

## ◆ Measured

- eddy flux (short term)
- evaporation pans (long term)

## ◆ Computed from mass transfer formulae

$$E = \rho f(W_z) (e_s - e_z) \quad \text{Dalton's Law}$$

$e_s$  = vapor pressure at surface

$e_z$  = vapor pressure at elevation  $z$

$$f(W_z) = \text{wind speed function} = a + bW_z \quad (k_g)$$

# Evaporative Heat Flux (cont'd)

- ◆ Mass transfer => heat transfer using latent heat of vaporization

$$L_v = (2493. - 2.26T_s) \times 10^3 \quad \text{J/Kg}$$

$$\phi_e = L_v E = f(W_z)(e_s - e_a)$$

$$\phi_e = 3.72W_2(e_s - e_2)$$

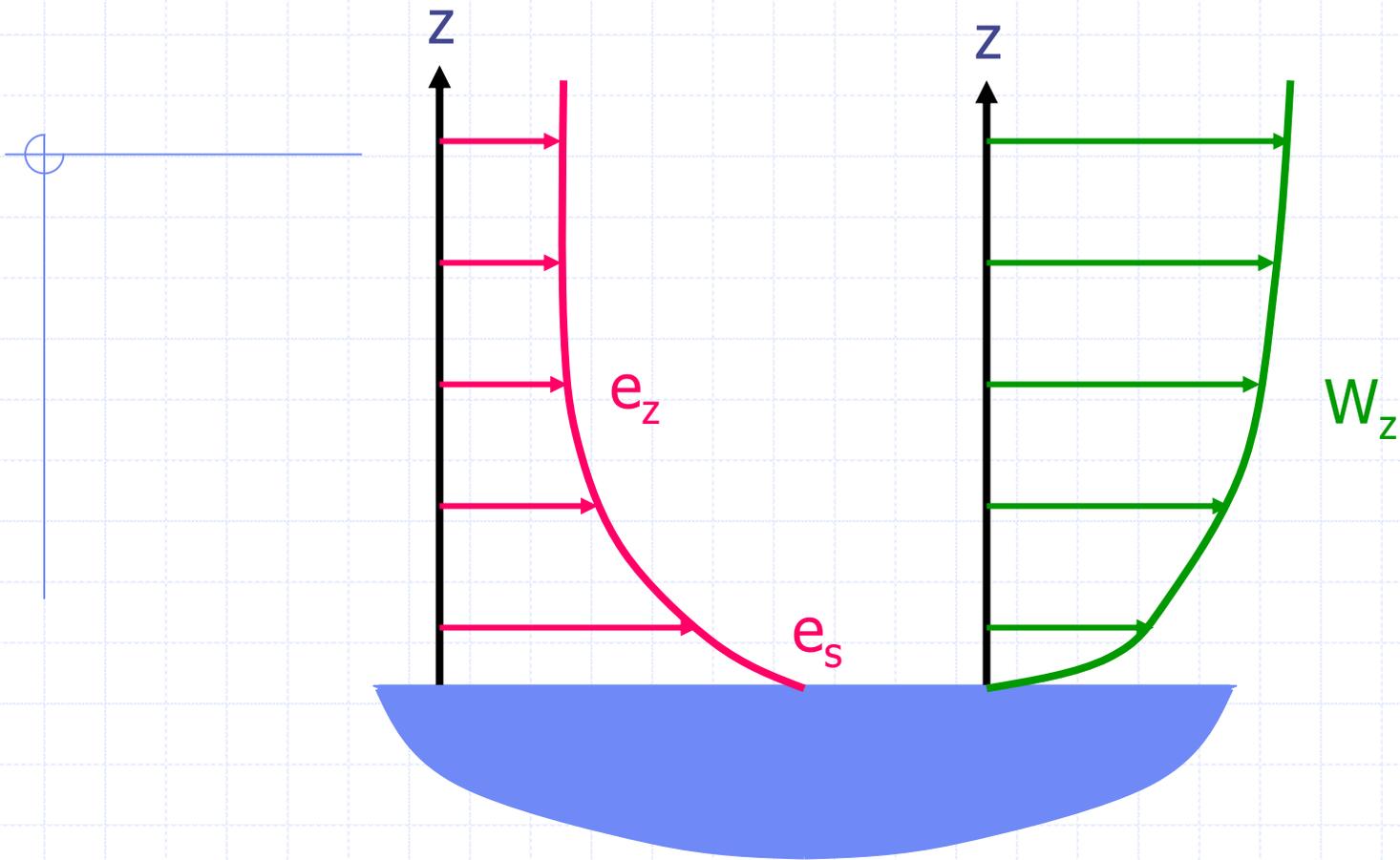
“Lake Hefner”, Marciano and Harbeck (1954)

(W/m<sup>2</sup>; W<sub>2</sub> in m/s; e<sub>s</sub>, e<sub>2</sub> in mb)

$$\phi_e = 5.1A^{-0.05}W_2(e_s - e_2)$$

“Fetch-dependence”  
Harbeck, (1962)

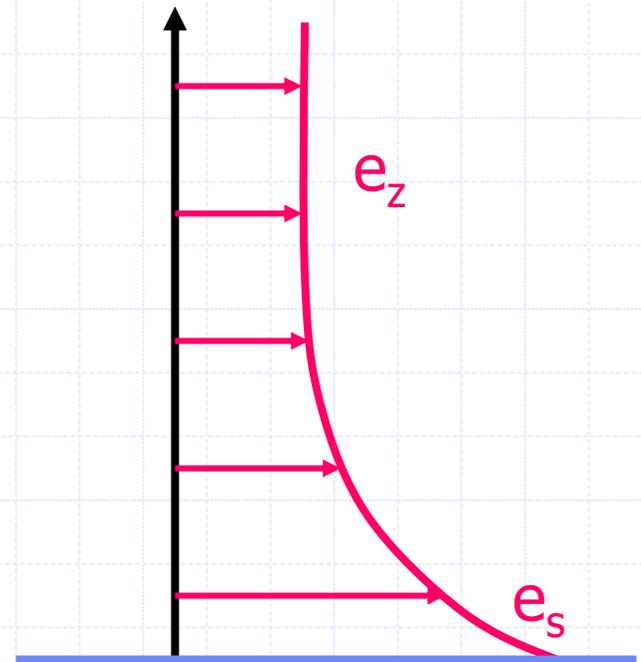
(A in ha)



$e_z$  and  $W_z$  vary vertically (height above water) and horizontally (above water or on-shore)

# Evaporation from non-natural water bodies

- ◆  $e_s$  increases with temperature
  - Heated water bodies have increased evaporation (water vapor also lighter than air)
- ◆  $e_s$  decreases with salinity
  - Saline bodies have decreased evaporation
- ◆  $e_s$  decreases with pressure



$$\phi_e = f(W_z) (e_s - e_z)$$

# Conductive Heat Flux

- ◆ Computed from evaporative flux using Bowen Ratio

$$\phi_c = R_b \phi_e$$

$$R_b = C_b \frac{(T_s - T_z)}{(e_s - e_z)}$$

$$C_b = 0.61 \text{ mb/}^\circ\text{C};$$

# Summary

$$\phi_n = \phi_{sn} + \phi_{an} - \underbrace{\phi_{br} - \phi_e - \phi_c}_{\text{functions of } T_s}$$

functions of external factors (met  
and astronomical conditions)

Strategies for computation: table look up

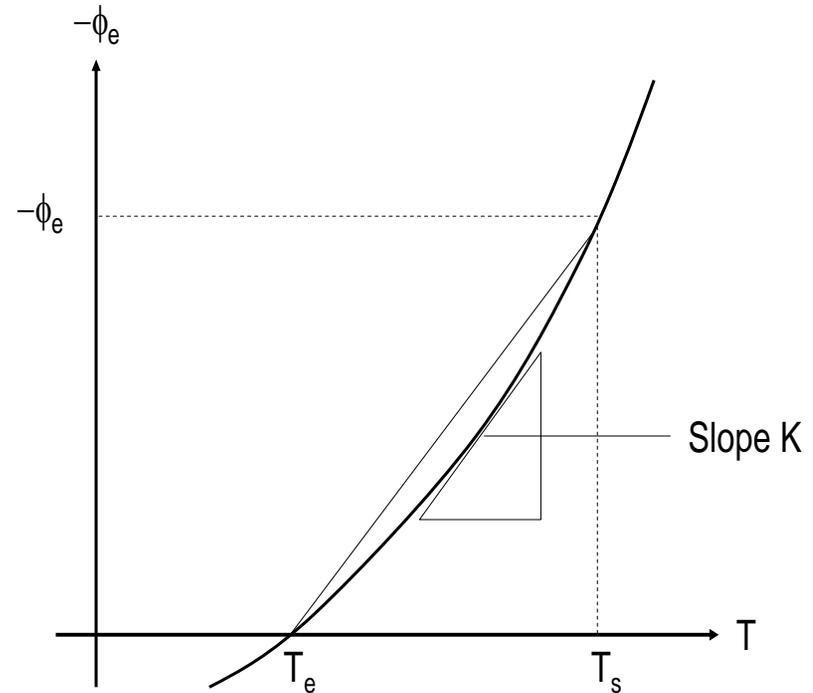
Self regulation: errors in calculations compensate

# Linear Heat Transfer

- ◆ Equilibrium Temp,  $T_e$ 
  - $T_s$  for which  $\phi_n = 0$
  - Function of met
- ◆ Surface Heat Exchange Coefficient,  $K$ 
  - Slope of  $\phi_n$  vs  $T_s$

$$\phi_n = -K(T_s - T_e)$$

$$K \sim 20-50 \text{ W/m}^2\text{°C}$$



# Example: Periodic Heat Loss

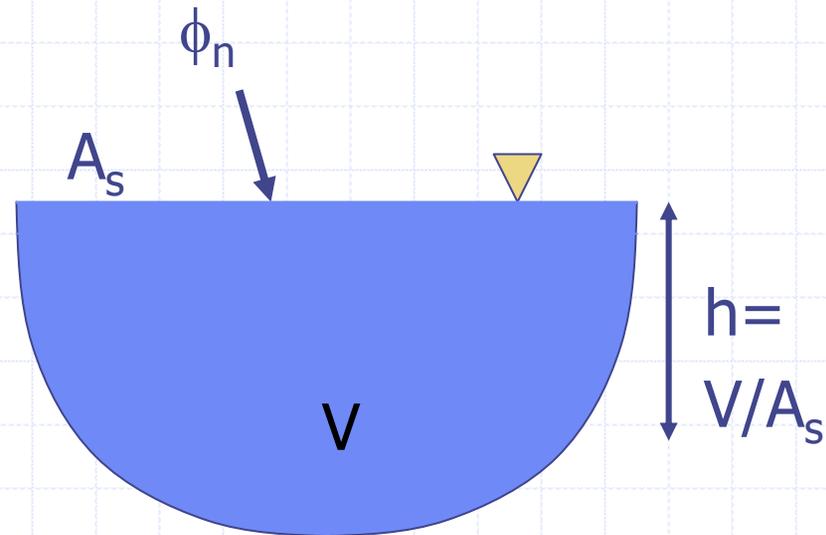
$$\rho c V \frac{dT}{dt} = A_s \phi_n$$

$$\frac{dT}{dt} = -k(T - T_e) \quad k = K/\rho c_p h$$

$$T_e = \bar{T}_e + \Delta T_e e^{i\omega t} \quad \omega = 2\pi/P$$

$$T = \bar{T} + \Delta T * e^{i\omega t}$$

$$T = \bar{T}_e + \Delta T e^{i\theta} e^{i\omega t}$$



# Periodic Heat Loss (cont'd)

$$T = \bar{T} + \Delta T * e^{i\omega t}$$

$$\Delta T^* = \Delta T e^{i\theta}$$

$$T = \bar{T}_e + \Delta T e^{i\theta} e^{i\omega t}$$

$$T = \bar{T}_e + \Delta T e^{i\omega(t-t_L)}$$

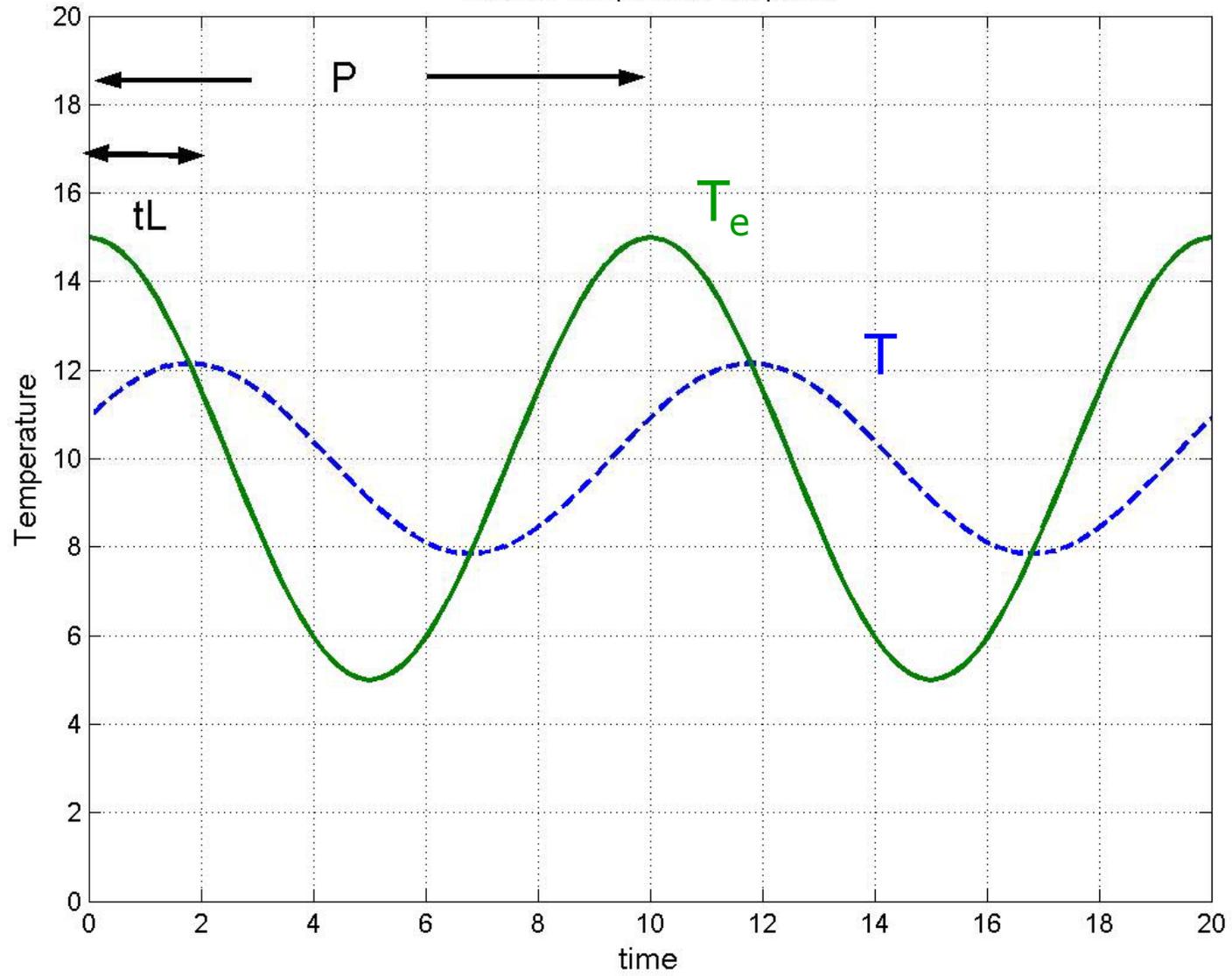
$$t_L = (\theta/2\pi)P$$

$$\frac{\Delta T^*}{\Delta T_e} = \frac{k}{k + i\omega} = \underbrace{\frac{k}{\sqrt{k^2 + \omega^2}}}_{\text{Amplitude}} e^{\underbrace{i \tan^{-1}(-\omega/k)}_{\text{Phase lag}}}$$

$$\theta = \tan^{-1}(-\omega/k)$$

$$t_L = \frac{P}{2\pi} \tan^{-1}(\omega/k)$$

Periodic Temperature Response



# Examples

$K/\rho c = 1\text{m/d}^*$ ;  $h = 10\text{m}$ ,  $k=K/\rho ch = 0.1\text{d}^{-1}$

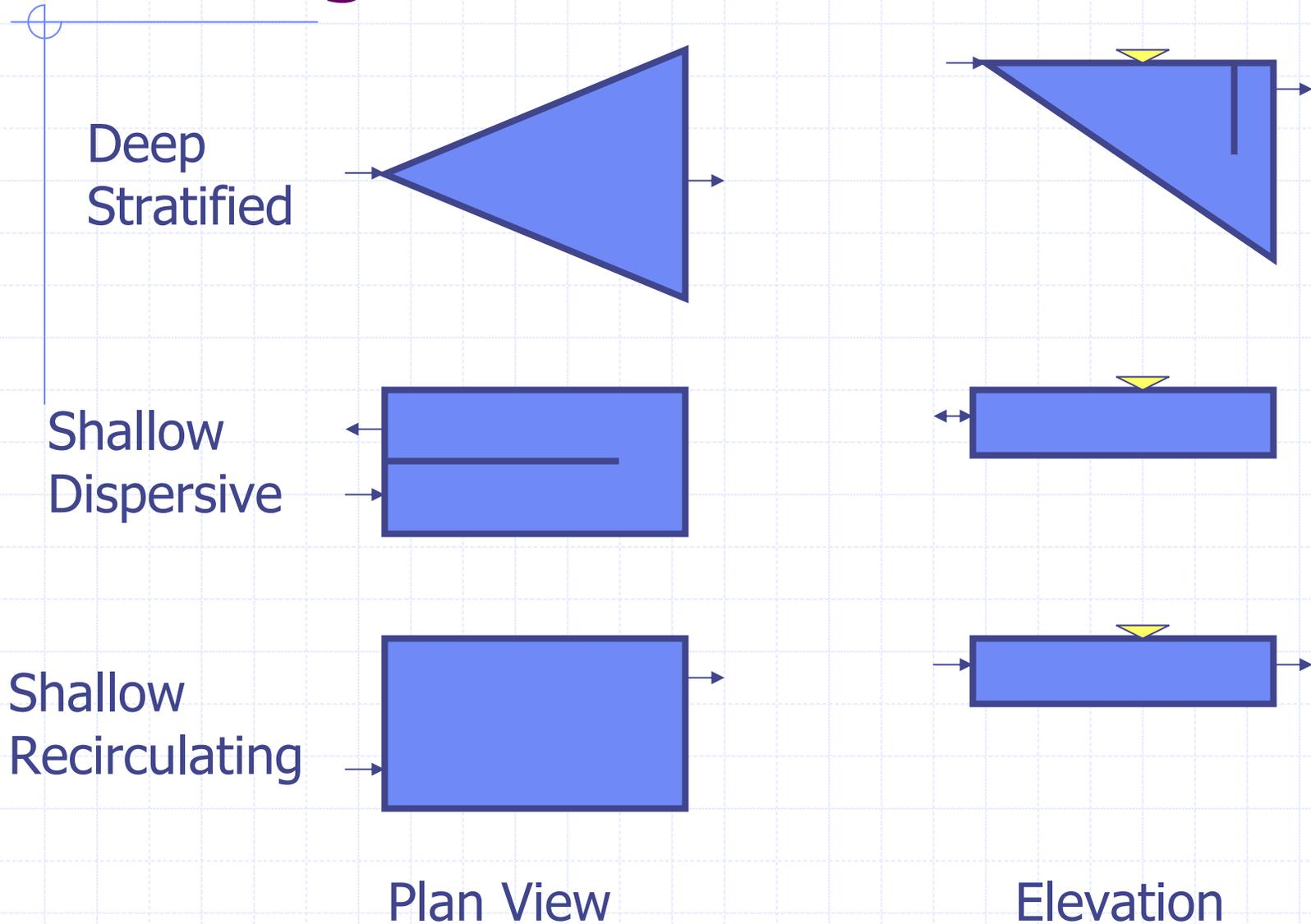
P	1 day	365
$\omega=2\pi/P$	$0.17\text{d}^{-1}$	$6.28\text{d}^{-1}$
$\Delta T/\Delta T_e$ $=k/(k^2+\omega^2)^{0.5}$	0.016	0.986
$\theta=\tan^{-1}(-\omega/k)$	$-89^\circ$	$-10^\circ$
$t_L =$ $P/2\pi\tan^{-1}(\omega/k)$	0.247 d	10 d

\*  $K \sim 48 \text{ W/m}^2\text{C}$

# Cooling Lakes and Ponds

- ◆ Used to cool electric power plants
- ◆ Shallow (vertically well-mixed)
  - Erected with dikes
  - $T = T(x,y) + T(t)$
- ◆ Deep reservoirs
  - Damming of reservoirs
- ◆ Cooling capacity
  - $r = KA_p / \rho c Q_o$

# Cooling Ponds



# Example: shallow-longitudinal dispersive

$$\rho c Q_o \frac{dT}{dx} = \rho c W H E_L \frac{d^2 T}{dx^2} - K(T - T_E) W$$

Single pass

$$\frac{T_i - T_E}{T_o - T_E} = \frac{4ae^{1/2E_L^*}}{(1+a)^2 e^{a/2E_L^*} - (1-a)^2 e^{-a/2E_L^*}}$$

Continuous operation

$$(T_o = T_i + \Delta T_o)$$

$$\frac{T_i - T_E}{\Delta T_o} = \frac{4ae^{1/2E_L^*}}{(1+a)^2 e^{a/2E_L^*} - (1-a)^2 e^{-a/2E_L^*} - 4ae^{1/2E_L^*}}$$

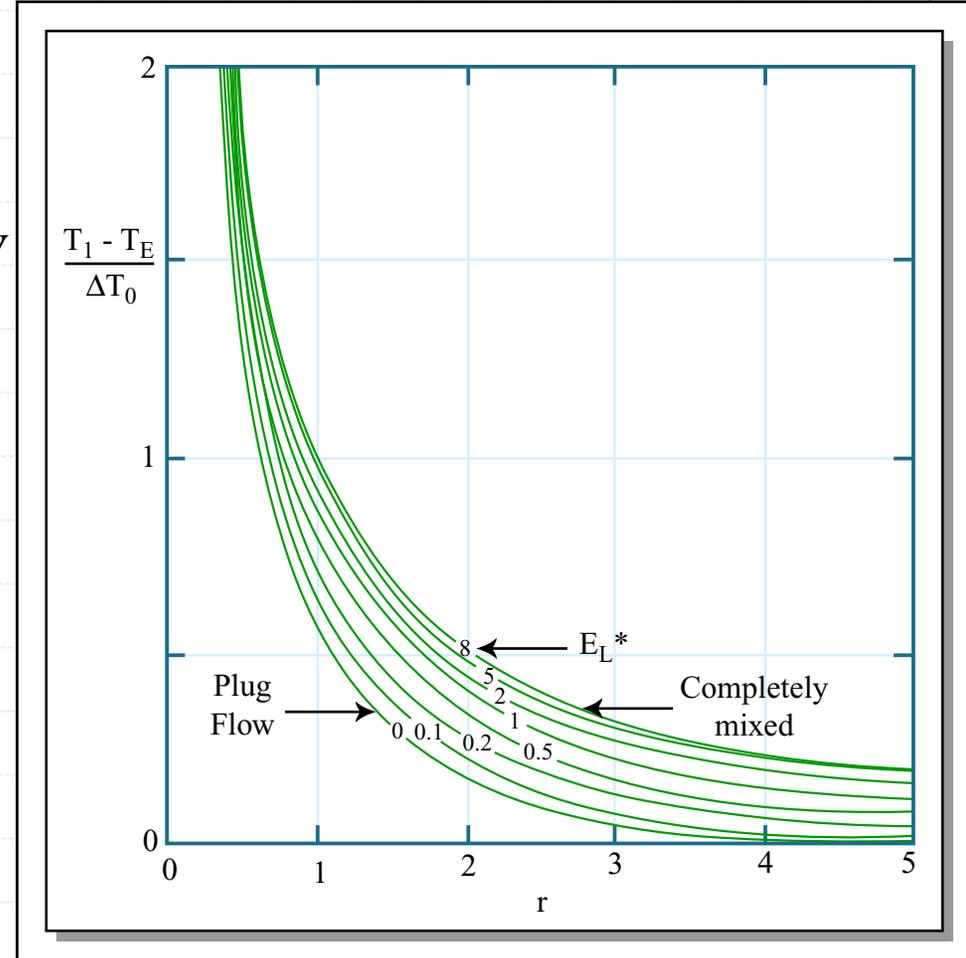


Figure by MIT OCW.

# Stratification in Lakes & Reservoirs

## ◆ Factors causing vertical stratification

- Differential absorption
- Reduced vertical mixing

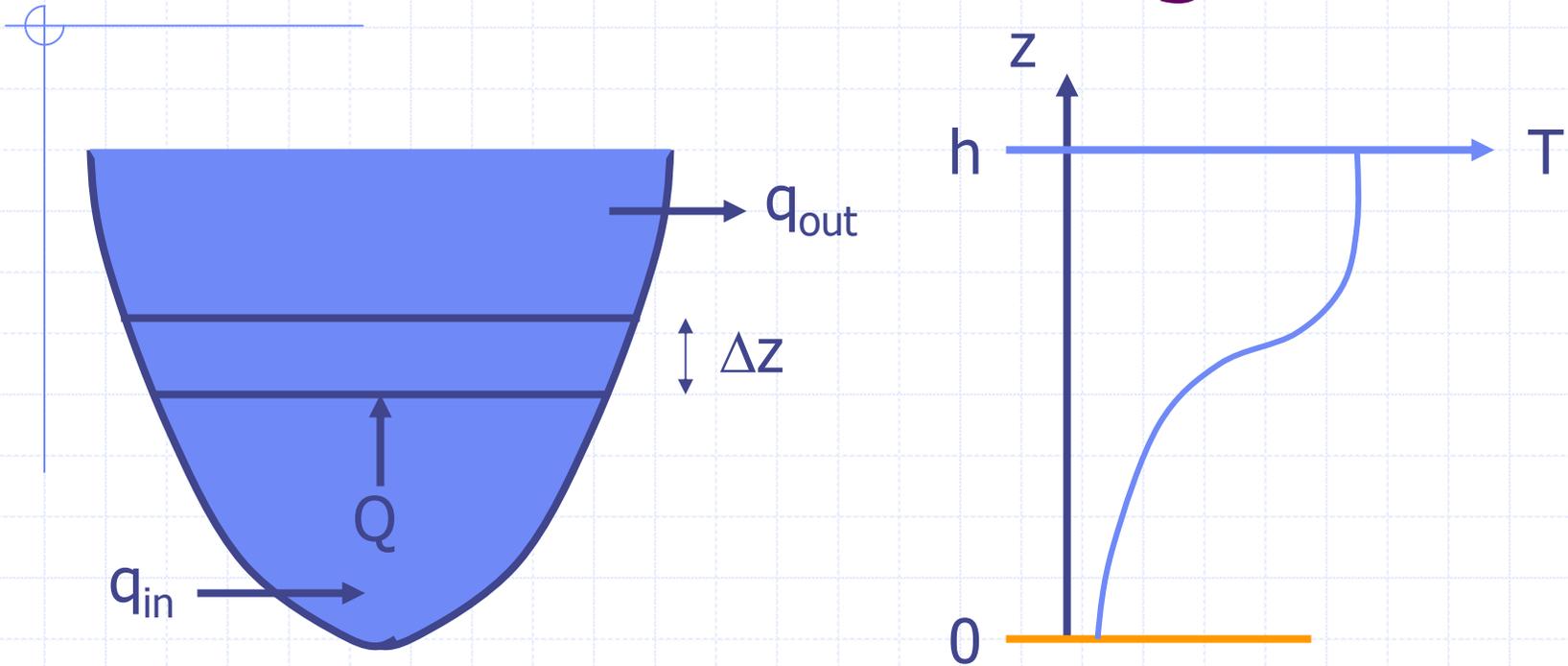
## ◆ Factors causing horizontal stratification

- Strong through flow
- Strong wind
- Differential absorption

# Reservoir classification based on horizontal through flow (Orlob, 1969)

- ◆ Through flow velocity =  $L/(V/Q)$
- ◆ Int'l wave speed  $\sim (g\Delta\rho/\rho h)^{0.5} \sim Nh$ 
  - $N$  = buoyancy freq =  $[(g/\rho)(d\rho/dz)]^{0.5}$
  - $L$  = length;  $Q$  = flow;  $h$  = depth;  $V$  = vol
- ◆  $F_r = LQ/VNh$ 
  - $F_r \ll 1$  vertically stratified
  - $F_r \gg 1$  vertically mixed

# 1-D Reservoir Modeling

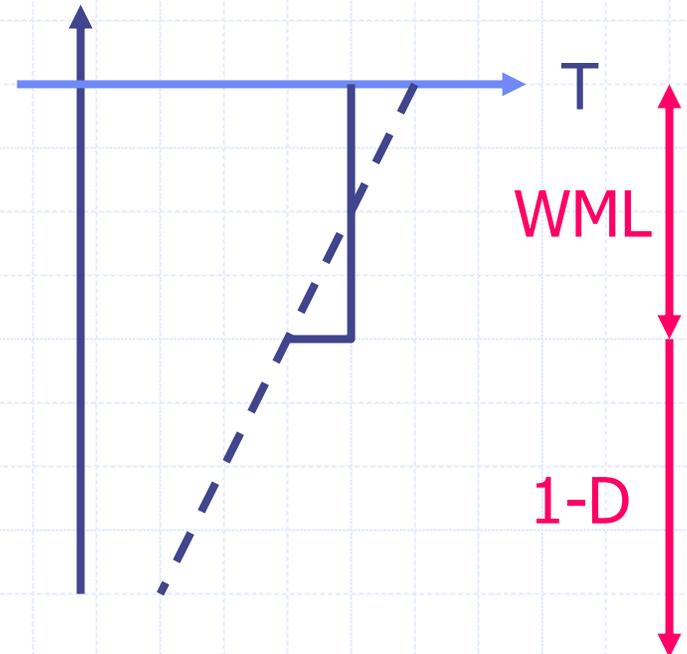


$$\frac{\partial Q}{\partial z} = q_{in} - q_{out}$$

$$\frac{\partial T}{\partial t} + \frac{1}{A} \frac{\partial}{\partial z} (QT) = \frac{1}{A} \frac{\partial}{\partial z} \left[ AE_z \frac{\partial T}{\partial z} \right] + \frac{q_{in} T_{in} - q_{out} T}{A}$$

# Surface Layer

- ◆ Well mixed layer
  - Convective mixing
  - Wind mixing
- ◆ Wind mixing algorithm for surface
  - Oceans (Kraus-Turner)
- ◆ 1-D model below



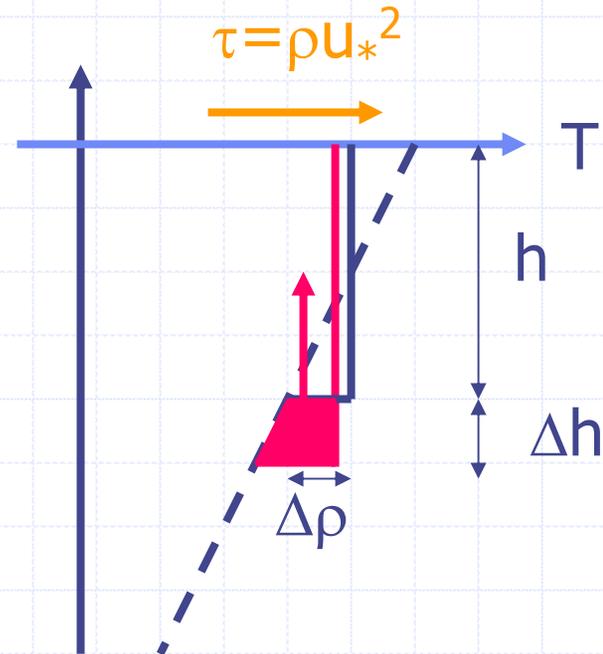
# Surface Layer (cont'd)

$$\frac{\Delta PE}{A} = (\Delta\rho g \Delta h) \frac{h}{2} = \frac{\Delta\rho g h}{2} u_e \Delta t$$

$$\frac{\Delta KE}{A} = \rho u_*^2 u_s \Delta t \sim \rho u_*^3 \Delta t$$

$$\frac{\Delta PE}{\Delta KE} = \text{const}$$

$$\frac{u_e}{u_*} \sim \frac{u_*^2}{\frac{\Delta\rho}{\rho} g h} = Ri^{-1}$$



Many variants

# Lake stability

Stability index (PE of water body with equivalent mass and heat content but uniform density – PE of stratified body)

$$SI = \int_0^h [\bar{\rho} - \rho(z)][z - z_c] g A(z) dz$$

$$\bar{\rho} = \int_0^h \rho(z) A(z) dz \Big/ \int_0^h A(z) dz \quad \text{Average density}$$

$$z_c = \int_0^h \rho(z) A(z) z dz \Big/ \int_0^h \rho(z) A(z) dz \quad \text{Center of mass}$$