

Recitation 7 - Problems

April 6th and 7th

Problem 1

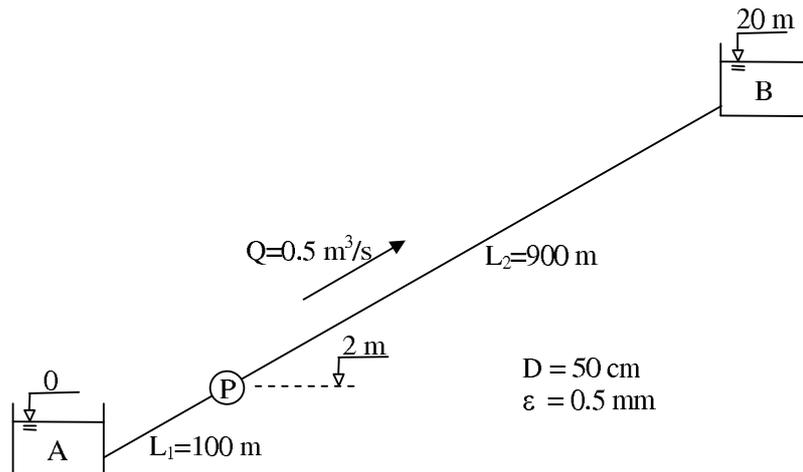


Figure 1: Pump impulsion in Problem 1.

A water flowrate $Q = 0.5 \text{ m}^3/\text{s}$ is being pumped from a large reservoir A , where the free surface elevation is $z = 0$, to a large reservoir B , where the free surface elevation is $z = 20 \text{ m}$. The pipe that connects the two reservoirs has diameter $D = 50 \text{ cm}$ and roughness $\epsilon = 0.5 \text{ mm}$. The pump is located at elevation $z = 2 \text{ m}$. The pipe length between A and the pump is $L_1 = 100 \text{ m}$ and the pipe length between the pump and B is $L_2 = 200 \text{ m}$. These characteristics are represented in Figure 1. Neglect minor losses.

- Determine the pump head, H_p , necessary to pump the indicated flowrate.
- If the required NPSH of the pump is 6 m , would you worry about cavitation in the pump? Assume that the temperature is 20°C .
- Draw the energy grade line (EGL), specifying the relevant values.
- The efficiency of the pump is $\eta = 0.8$ and the cost of electricity is 10 cents per kWh . How much does it cost to pump 1 m^3 (258.1 gallons) from A to B ?

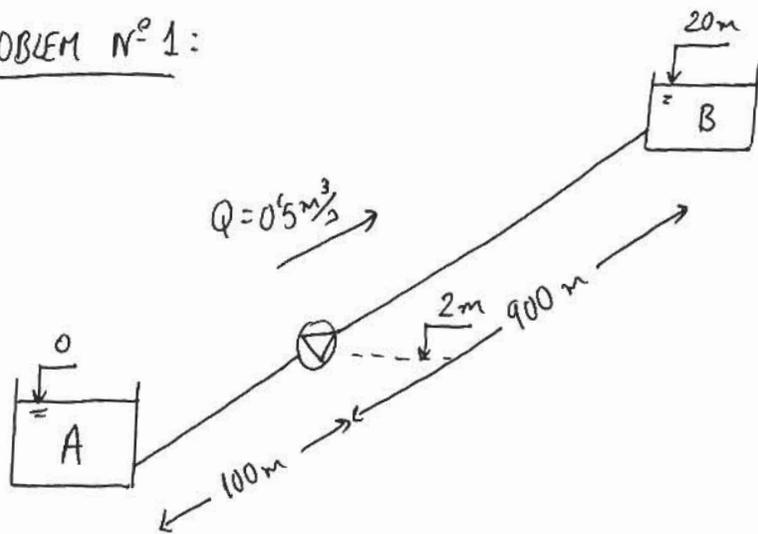
Problem 2

A sphere of diameter $D = 0.075 \text{ m}$ and weight $W = 1.37 \text{ N}$ is moving through air ($\rho_a = 1.2 \text{ kg/m}^3$, $\nu_a = 1.5 \cdot 10^{-5} \text{ m}^2/\text{s}$) at a speed of $V_p = 42.5 \text{ m/s}$ (95 mph).

- a) What is the kinetic energy of the sphere?
- b) What is the Reynolds number upon which the sphere's coefficient, C_D , depends?
- c) If $C_D = 0.3$, determine the drag force, F_D , acting on the sphere as it moves through the air.
- d) Determine the rate at which the sphere loses kinetic energy due to the air resistance.
- e) Assuming the rate of loss of kinetic energy determined in **(d)** to remain constant, estimate the velocity of the sphere 0.4 s after it was given the initial velocity $V_p = 42.5 \text{ m/s}$.

RECITATION 7 - SOLUTIONS

- PROBLEM N° 1:



$$D = 0.5 \text{ m}$$

$$\epsilon = 5 \cdot 10^{-4} \text{ m}$$

a)

Apply Bernoulli between A and B:

$$H_A + H_p = H_B + \Delta H_{\text{losses}}$$

$$H_A = 0, H_B = 20 \text{ m}, \Delta H_{\text{losses}} = \Delta H_f = f \frac{L}{D} \frac{V^2}{2g} \quad (\text{Minor losses neglected})$$

$$V = \frac{Q}{\pi D^2/4} = \frac{0.5}{\pi \cdot 0.5^2/4} = 2.55 \text{ m/s} \rightarrow Re = \frac{VD}{\nu} = \frac{2.55 \cdot 0.5}{10^{-6}} = 1.3 \cdot 10^6$$

$$\frac{\epsilon}{D} = \frac{5 \cdot 10^{-4}}{0.5} = 10^{-3} \quad \left. \begin{array}{l} \text{MOODY} \\ \rightarrow f = 0.020 \end{array} \right\}$$

$$\Delta H_{f1} = 0.020 \cdot \frac{100}{0.5} \cdot \frac{2.55^2}{2 \cdot 9.8} = 1.33 \text{ m} \quad (\text{Headloss from A to pump})$$

$$\Delta H_{f2} = 0.020 \cdot \frac{900}{0.5} \cdot \frac{2.55^2}{2 \cdot 9.8} = 11.94 \text{ m} \quad (\text{Headloss from pump to B})$$

$$\underline{H_p} = H_B - H_A + \Delta H_{fA \rightarrow B} = 20 - 0 + (1.33 + 11.94) = \underline{\underline{33.3 \text{ m}}}$$

b)

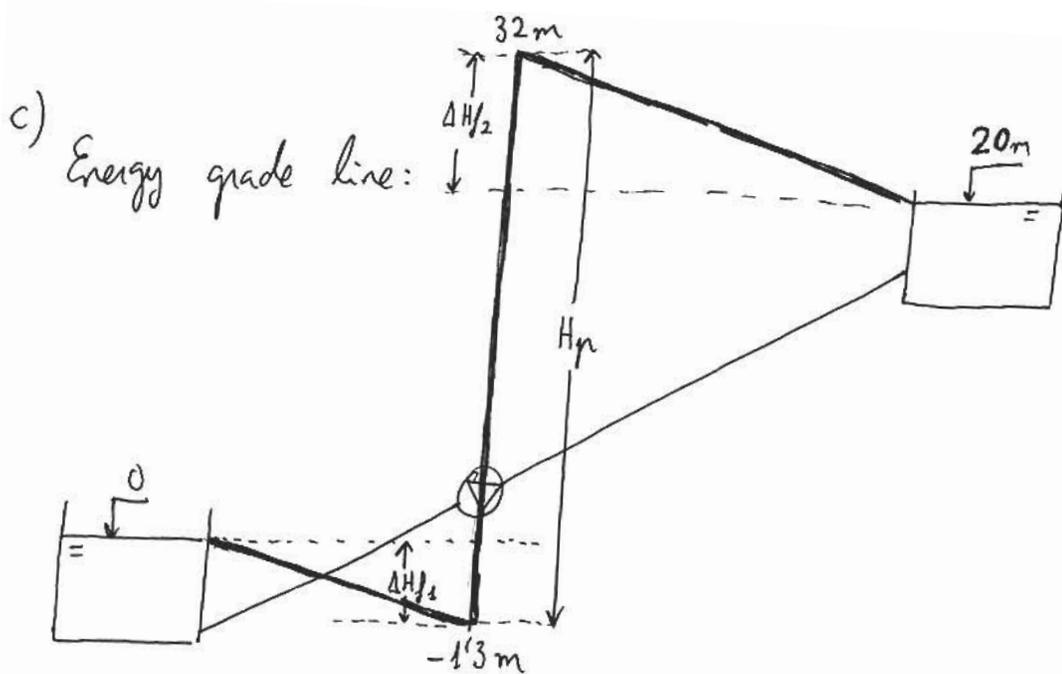
$$NPSH = \frac{V^2}{2g} + \frac{p - p_{\text{vapor, gauge}}}{\rho g} = H - z_{\text{pump}} - \frac{p_{\text{vapor, gauge}}}{\rho g} =$$

↑
head at the pump location

$$= (H_A - \Delta H_{f1}) - z_{\text{pump}} - \frac{p_{\text{vapor, gauge}}}{\rho g} = (0 - 1.33) - 2 - \frac{(2338 - 101300)}{9800} =$$

↙ 20°C

$$= 6.77 \text{ m} > NPSH_{\text{ref}} = 6 \text{ m} \Rightarrow \underline{\underline{NO CAVITATION}}$$



d)

$$\text{BHP} = \frac{\rho g Q H_p}{\eta} = \frac{9800 \cdot 0.5 \cdot 33.3}{0.8} = 163200 \text{ W} = 163 \text{ kW}$$

$$\text{Volume lifted in 1 hour} = 0.5 \frac{\text{m}^3}{\text{s}} \cdot 3600 \frac{\text{s}}{\text{h}} = 1800 \frac{\text{m}^3}{\text{h}}$$

$$\text{Cost per cubic meter} = \frac{163 \text{ kW} \cdot 10 \frac{\text{¢}}{\text{kWh}}}{1800 \frac{\text{m}^3}{\text{h}}} = \underline{\underline{0.91 \frac{\text{cents}}{\text{m}^3}}}$$

Problem No: 2

a)

$$W = m \cdot g = m \cdot 9.8 = 1.37 \text{ N} \Rightarrow m = \text{mass of sphere} = 0.14 \text{ kg}$$

$$E_{\text{kin},0} = \frac{1}{2} m V_p^2 = \underline{126 \text{ (Nm = Joule)}}$$

b)

$$Re = D V_p / \nu_a = 0.075 \cdot 42.5 / (1.5 \cdot 10^{-5}) = \underline{2.1 \cdot 10^5}$$

c)

$$F_D = \frac{1}{2} \rho_a C_D A_L V_p^2 \text{ (from cheat sheet)} = \frac{1}{2} \cdot 1.2 \cdot 0.3 \cdot \frac{\pi}{4} (0.075)^2 (42.5)^2$$

$$\underline{F_D = 1.44 \text{ N}} \quad [\text{notice } F_D \approx W]$$

d)

Rate at which work is done against drag force =

$F_D \cdot V_p$ = Rate at which sphere loses energy

$$\underline{\dot{E}_{\text{loss}}} = 1.44 \cdot 42.5 = \underline{61.0 \text{ (Nm/s = Joules/s = Watts)}}$$

e)

Energy lost after 0.4s flight = $E_{\text{loss}} \cdot 0.4 = 24.4 \text{ Joules}$

Remaining $E_{\text{kin}} = E_{\text{kin},0} - \dot{E}_{\text{loss}} \cdot 0.4 = 126 - 24.4 = 101.6 \text{ Joules}$

$$\frac{1}{2} m V_{0.4}^2 = \frac{1}{2} \cdot 0.14 \cdot V_{0.4}^2 = 101.6 \Rightarrow \underline{V_{0.4}} = \underline{\left(2 \cdot 101.6 / 0.14\right)^{1/2}} = \underline{38.1 \text{ m/s}}$$

[Note reduction in velocity = $42.5 - 38.1 = 4.4 \text{ m/s} = 9.8 \text{ mph}$

Baseball rule of thumb: Pitch velocity crossing the plate is $\sim 10 \text{ mph}$ slower than when it leaves the pitcher's hand].