

Lecture 13: Thermodynamics of Free Radical Polymerizations, Ceiling T's, Tromsdorff Effect, Instantaneous P_n

Thermodynamics (Continued)

$$\Delta H^\circ - T\Delta S^\circ = \Delta G^\circ = -RT \ln K_{eq}$$

$$\Delta G = \Delta G^\circ + RT \ln K_{eq} \quad \text{in general}$$

but at equilibrium:

$$\Delta G = 0 = \Delta G^\circ + RT \ln K_{eq}$$

$$\text{so } \Delta H^\circ - T_c \Delta S^\circ = -RT_c \ln \frac{1}{[M]_c} \quad \text{at equilibrium}$$

where $[M]_c$ = ceiling monomer con'c

Solve for T_c :

$$T_c = \frac{\Delta H^\circ}{\Delta S^\circ + R \ln [M]_c}$$

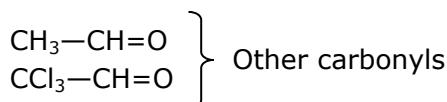
$$[M]_c = \frac{[M]_{eq}}{[M]_s^0} \quad \begin{array}{l} \xleftarrow{\hspace{1cm}} \text{Equilibrium} \\ \xleftarrow{\hspace{1cm}} \text{S.S. in mol/L (standard state in mol/L)} \end{array}$$

$[M]_s^0 \Rightarrow$ bulk concentration of monomer or 1 mol/L (depending on who's defining it)
We will use 1 mol/L

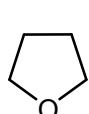
Susceptible polymers for “unzipping”

Carbonyl: $\text{CH}_2=\text{O}$

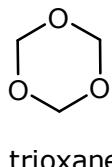
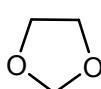
e.g. $-\text{CH}_2-\text{O}-$ unzips to form formaldehyde



Cyclics:

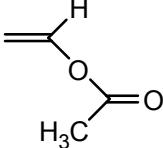
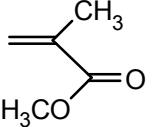
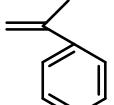


THF



trioxane

unzips via $-\left(\overset{\text{H}_2}{\text{C}}-\text{O}\right)_n-$ as well

Monomer	[M] _c @ 25°C (mol/L)	T _c (pure monomer) (°C)
Vinyl acetate 	1x10 ⁻⁹	~ 400°C or higher
Methyl metacrylate (MMA) 	1x10 ⁻³	220°C
α-methyl styrene 	2.2	61°C

Polydispersity Index (PDI) for Free Radical Polymerization

$$\nu = \frac{R_p}{R_t} = \frac{k_p[M]}{k_t[M \cdot]} = (\text{for thermally diss. initiator}) = \frac{k_p[M]}{(2k_d f k_t [I])^{\frac{1}{2}}}$$

$$\overline{p_n} = 2a\nu$$

Statistical Approach

p = probability of growth of polymer chain
= "propagation probability"

$$p = \frac{k_p[M]}{k_p[M] + 2k_t[M \cdot]} = \frac{R_p}{R_p + R_t (+ R_{tr})}$$

if needed (for chain transfer)

1-p = probability of chain termination

$$1-p = \frac{2k_t[M \cdot]}{k_p[M] + 2k_t[M \cdot]}$$

X_i = number fraction of radicals having reached degree of polymerization = i

$$X_i = p^{(i-1)} \underbrace{(1-p)}_{\text{for chain end}}$$

$$\overline{p_n} = \frac{\sum_{i=1}^{\infty} iX_i}{\sum X_i} = \sum_{i=1}^{\infty} iX_i = (1-p) \sum_{i=1}^{\infty} ip^{(i-1)} \quad \text{apply series definition}$$

1.0

$$\Rightarrow \boxed{\overline{p_n} = \frac{1}{1-p}} \quad \left. \right\} \text{here } p \neq \pi \text{ as in step growth}$$

$$\text{now } p = \frac{R_p}{R_p + R_t}$$

$$\overline{p_n} = \frac{1}{1-p} = \frac{R_p + R_t}{R_t}$$

as $p \rightarrow 1.0$ (i.e. $R_p \gg R_t$)

$$\Rightarrow \overline{p_n} \rightarrow \nu$$

$$\Rightarrow \overline{p_n} \rightarrow \frac{R_p}{R_t}$$

$$\overline{p_w} = \sum iWi = \frac{\sum i^2Xi}{\sum iXi} = \frac{\sum i^2Xi}{\overline{p_n}} \quad \text{apply series defn}$$

weight fraction

$$\Rightarrow \boxed{\overline{p_w} = \frac{1+p}{1-p}}$$

PDI: $z = 1+p$ } disproportionation

as $p \rightarrow 1.0$
 $z \rightarrow 2.0$

This all assumes termination by disproportionation
If we assume coupling, account for $\sim X \cdot + \cdot Y \sim$

$$\begin{aligned} \Rightarrow \overline{p_n} &= \frac{2}{1-p} \\ \overline{p_w} &= \frac{2+p}{1-p} \\ z &= \frac{\overline{p_w}}{\overline{p_n}} = \frac{2+p}{2} \end{aligned} \quad \left. \right\} \quad \text{as } p \rightarrow 1.0 \quad z \rightarrow 3/2$$

Instantaneous vs. Integrated Rate Expressions

$$R_p = k_p \left(\frac{f k_d}{k_t} \right)^{\frac{1}{2}} [I]^{\frac{1}{2}} [M] = -\frac{d[M]}{dt} \quad \text{instantaneous expression}$$

Express things in terms of π (monomer conversion)

$$\pi = \frac{[M]_o - [M]}{[M]_o} = 1 - \frac{[M]}{[M]_o}$$

$$\frac{d\pi}{dt} = -\frac{1}{[M]_o} \frac{d[M]}{dt}$$

$$\frac{d\pi}{dt} = k_p \left(\frac{f k_d}{k_t} \right)^{\frac{1}{2}} [I]^{\frac{1}{2}} [1 - \pi]$$

integrate assuming a constant $[I] = [I]_o$

$$\pi(t) = 1 - \exp \left[-k_p \left(\frac{f k_d}{k_t} \right)^{\frac{1}{2}} [I]_o t \right]$$

so applies to batch polymer $[M] \downarrow$
but $[I]$ constant \Rightarrow e.g. early stages of polymer

If $[I]$ is not held constant:

$$\frac{d[I]}{dt} = -k_d [I]$$

$$[I] = [I]_o \exp(-k_d t)$$

$$\frac{d\pi}{dt} = k_p \left(\frac{f k_d}{k_t} \right)^{\frac{1}{2}} [I]_o^{\frac{1}{2}} \exp \left(-\frac{k_d t}{2} \right) (1 - \pi)$$

Integrate from $t=0$ to t :

$$\pi_t = 1 - \exp \left\{ \left(\frac{2 k_p}{k_d} \right) \left(\frac{f k_d}{k_t} \right)^{\frac{1}{2}} [I]_o^{\frac{1}{2}} \left[\exp \left(-\frac{k_d t}{2} \right) - 1 \right] \right\}$$

global expression: time of conv \rightarrow conv at that time

$$[M], [I] \downarrow \Rightarrow R_p \downarrow$$

Max conversion is batch situation:

Let $t \rightarrow \infty$
So that all of I is consumed

$$\pi_{\max} = 1 - \exp \left\{ - \left(\frac{2k_p}{k_d} \right) \left(\frac{fk_d}{k_t} \right)^{\frac{1}{2}} [I]_o^{\frac{1}{2}} \right\}$$

e.g. Polystyrene, 1 wt% AIBN

$$\Rightarrow \pi_{\max} = 96.7\%$$

$$\overline{p_n} = f(t) \quad \overline{p_n} \text{ becomes fxn of time}$$

$$\overline{p_n}(t) = \frac{R_p(t)}{R_i(t)} \quad \begin{matrix} \leftarrow [M] \\ \leftarrow [I] \end{matrix}$$

$$\text{Time avg value: } \langle \overline{p_n}(t) \rangle = \frac{\text{tot mol of monomer polym}}{\text{tot mol of "dead" chains (formed)}} = \frac{a[M]_o \pi(t)}{f[I]_o (1 - \exp(-k_d t))}$$

(from $t=0 \rightarrow t$)

