

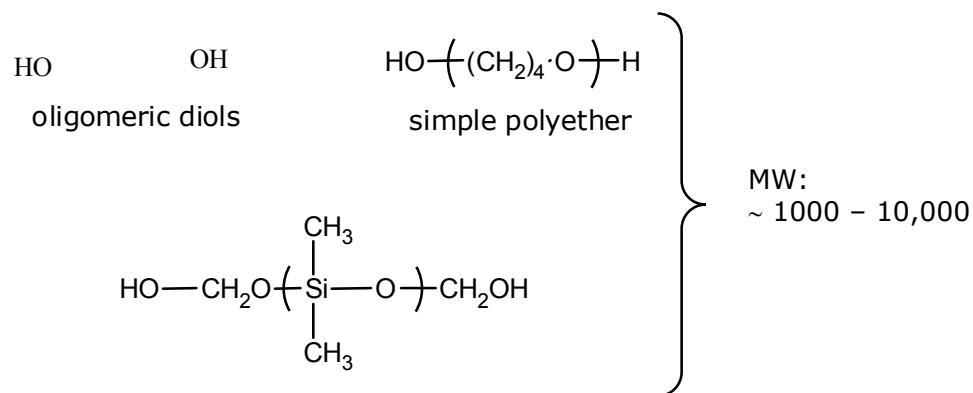
10.569 Synthesis of Polymers
 Prof. Paula Hammond
Lecture 10: Introduction to Radical Polymerization

Segmented Copolymers



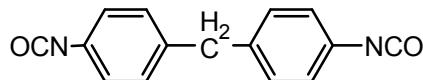
Segmented Polyurethanes (Prof. Hammond's thesis)

- ① "soft segment" → ends in -OH groups
 - oligomer
 - low T_g (liquid-like at 25°C)

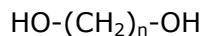


- ② Diisocyanate: (-N=C=O)

OCN-R-NCO
 e.g.
 $\text{OCN-(CH}_2\text{)}_6\text{-NCO}$

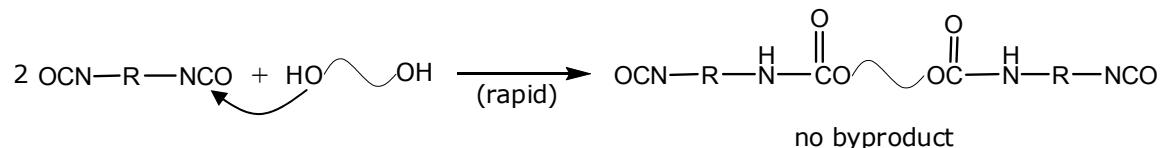


- ③ Chain extender
 - Connector between different units
 - Almost always short diol
 ex:



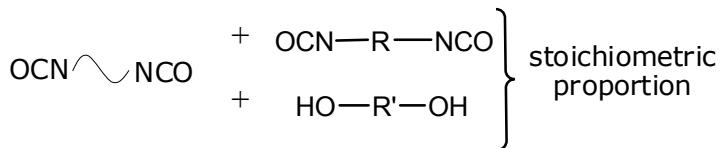
To get segmented polyurethane:

1. Endcap soft segment w/diisocyanate:

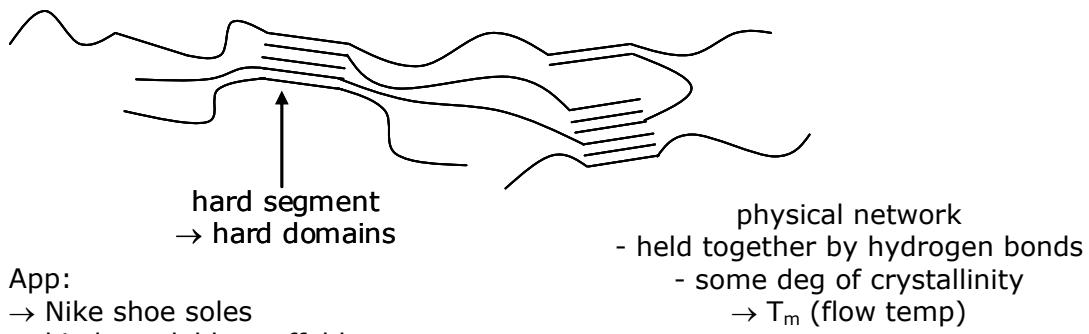


2.

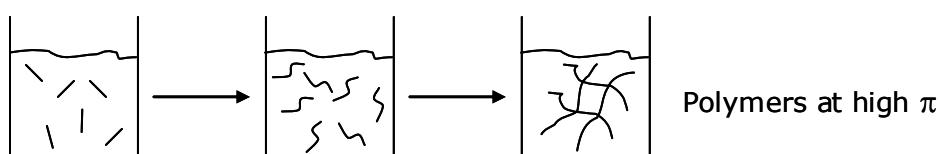
or



soft	isocyanate	chain extender	
1	2	1	$\left[\begin{array}{c} \text{O} & & \text{O} & & \text{O} & & \text{O} \\ \parallel & & \parallel & & \parallel & & \parallel \\ \text{O}-\text{C}-\text{H}-\text{N}-\text{R}-\text{N}-\text{C}-\text{O}-\text{R}'-\text{O}-\text{C}-\text{H}-\text{N}-\text{R}-\text{N}-\text{C}- \\ & & & & & & \\ \text{O} & & \text{O} & & \text{O} & & \text{O} \end{array} \right]$
1	3	2	Hard Segment
1	4	3	Can be made longer by adding diol and diisocyanate in equal proportions
-	-	-	$\left[\begin{array}{c} \text{---} \\ \\ \text{---} \end{array} \right]_3$
-	-	-	$\left[\begin{array}{c} \text{---} \\ \\ \text{---} \end{array} \right]_4$

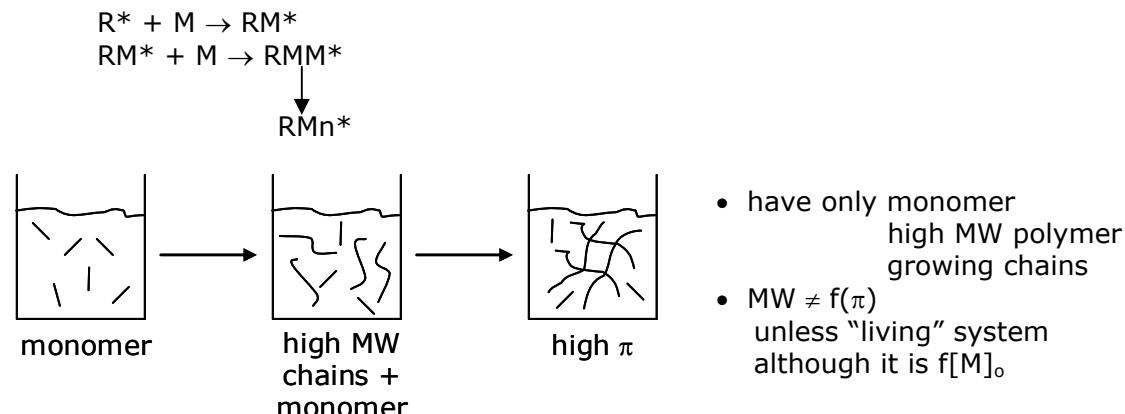


Step Growth Polymerization

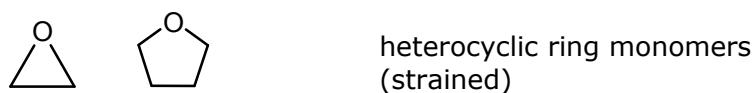


- 2nd order kinetics
- MW↑ linearly with time ($\overline{p}_n = 1 + [a]_0 kt$)
- $\text{MW} \propto \frac{1}{1-\pi}$
- All species in rxn bath are reactive
- Need high π for high MW
- monomer activation required for polymerization
- only activated monomer/polymer growing chains are active in rxn (v. small fraction at given time)
- growing chains get large rapidly then terminate, deactivates chain
- new monomer is activated

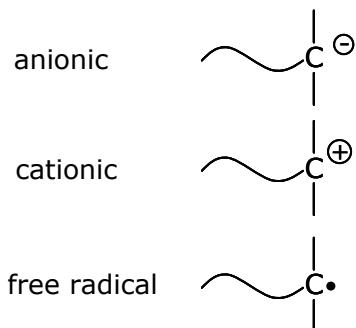
Chain Growth (Addition)



Addition monomers are:



Propagating (active) species:



Processes in Addition Polymerization:

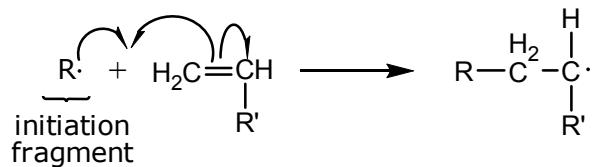
1. Initiation
2. Propagation
3. Termination
4. Transfer of charge or active species from one chain to another

(but not always present)

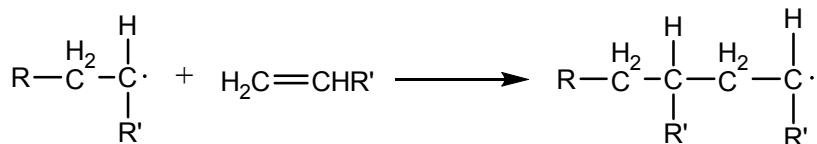
Free Radical Polymerization

Kinetics: $I \rightarrow 2R\cdot$

1. Initiation:



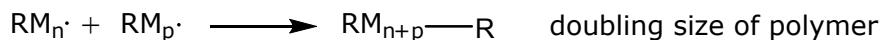
2. Propagation Step:



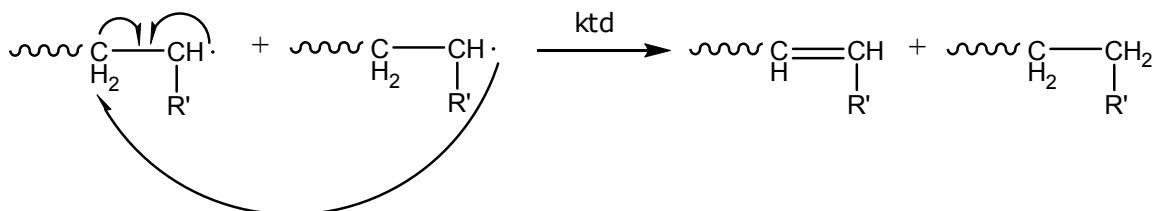
3. Termination:

Happens one of 2 ways:

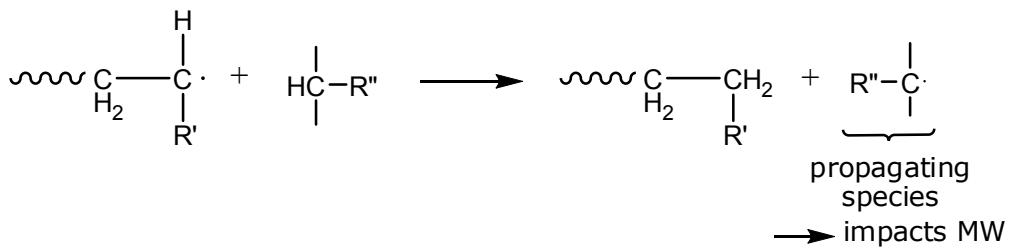
a. coupling



b. disproportionation



4. Chain Transfer:



Kinetic Rate Expression

Initiation:



$$\frac{d[\text{RM} \cdot]}{dt} = f \frac{d[\text{R} \cdot]}{dt}$$

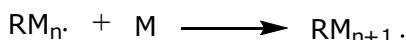
↑
efficiency factor

$$-\frac{d[\text{I}]}{dt} = k_d [\text{I}] = \frac{1}{2} \frac{d[\text{R} \cdot]}{dt}$$

↑
create 2 fragments

$$\frac{d[\text{RM} \cdot]}{dt} = f \frac{d[\text{R} \cdot]}{dt} = 2f k_d [\text{I}] k_d \sim 10^{-4} - 10^{-6} \frac{l}{\text{mol} \cdot \text{sec}}$$

Propagation



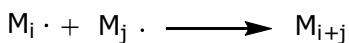
$$R_p = -\frac{d[M]}{dt} = k_p \underbrace{[M \cdot][M]}$$

$[M \cdot] \equiv [M_n \cdot]$ any active monomer

(assume equal reactivity for all $\text{M} \cdot$ species)

$$k_p \sim 10^2 - 10^4 \frac{l}{\text{mol} \cdot \text{sec}}$$

Termination



$$R_t = -\frac{d[M \cdot]}{dt} = 2k[M \cdot]^2$$

assume same disproportionation:

$$\text{let } k_t = k_{tc} + k_{td}$$

$$k_t \sim 10^6 - 10^8 \frac{l}{mol \cdot sec}$$

How fast are you creating polymer?

Polymerization rate

$$-\frac{d[M \cdot]}{dt} = R_p = k_p [M \cdot] [M]$$

Assume steady state free radical concentration $[M \cdot]$

$$\Rightarrow R_i = R_t$$

$$2k_t [M \cdot]^2 = 2k_d f[I]$$

Solve for $[M \cdot]$:

$$[M \cdot] = \left(\frac{k_d f[I]}{k_t} \right)^{\frac{1}{2}} \text{ plug into } R_p \text{ expression}$$

$$R_p = k_p \left(\frac{k_d f[I]}{k_t} \right)^{\frac{1}{2}} [M]$$

Generic Form:

$$R_p = \left(\frac{k_p^2}{2k_t} R_i \right)^{\frac{1}{2}} [M]$$