

**Lecture 6: Other Polymers of Interest obtained by Step-Growth,
Polyaramids, Polyimides, Segmented and Block Copolymers from Step
Condensation Methods**

Far from equilibrium polymerizations:

Processing: Bulk reactions much less desirable

- extremely reactive, exotherms huge
- high concentrations further increase R_p

Better to use solution polymerization:

- can control heat removal, viscosity
- controlled by solvent choice (high capacity or low capacity solvent)

Must consider solvent effects:

- solubility of both monomers
- solubility of high MW polymer
- wrong (poor) solvent can lead to low MW product

e.g. polyisocyanate

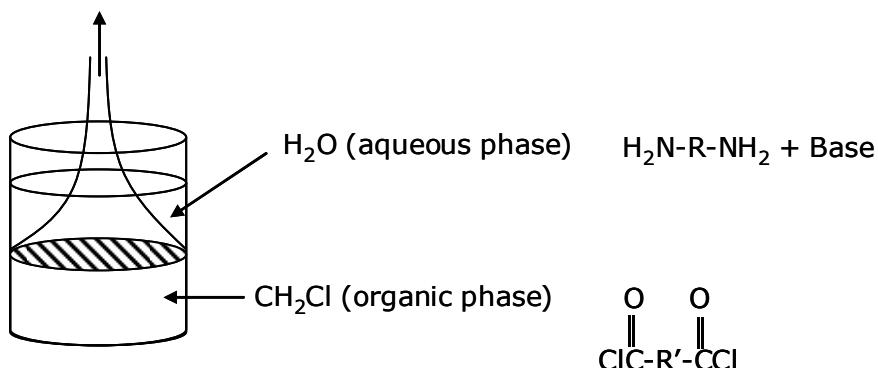
Inherent viscosity [dl/g, deciliter/gram]				
		Solvent	Polarity	η_{inh} (relative to MW)
hazardous		Xylene		0.06
		Chlorobenzene		0.17
		Nitrobenzene		0.36
	DMSO (used in many biological systems)			0.69

For specific case of fast polymerization:

- low temps are often desired
- $-40^{\circ}\text{C} \sim 80^{\circ}\text{C}$
- large ΔH_{exo} $\Rightarrow T \uparrow$ can lower $\pi \downarrow$
- at good conditions, it is very easy to get 100% π
- lower concentrations
- slow addition of monomer(s) \rightarrow control exotherm, prevent clumping

Alternatives to Solution Polymerization

Two Phase Polymerization



Draw polymer from interface

Interfacial Polymerization:

1. Reactants diffuse to interface
2. Immediate reaction → perfect stoichiometry at interface
Form high MW polymer
3. Remove polymer → fresh interface

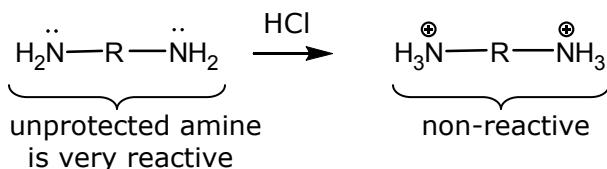
Polymerization continues until monomer is depleted in organic and/or H₂O phases.

Key Differences

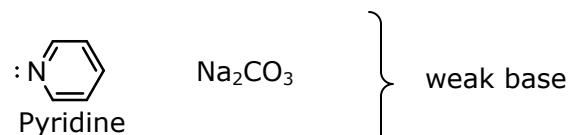
- Diffusion controlled (not kinetically)
- Bulk stoichiometry is irrelevant
- Treat 2 phases as reservoirs
- Higher concentrations in phases → higher mass transfer driving forces
- % conversion is not a factor in final MW

Details:

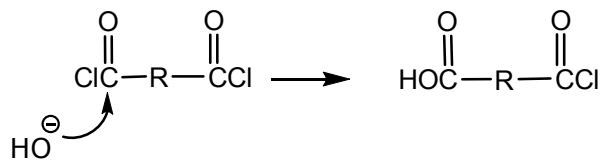
- addition of the base, HCl is generated



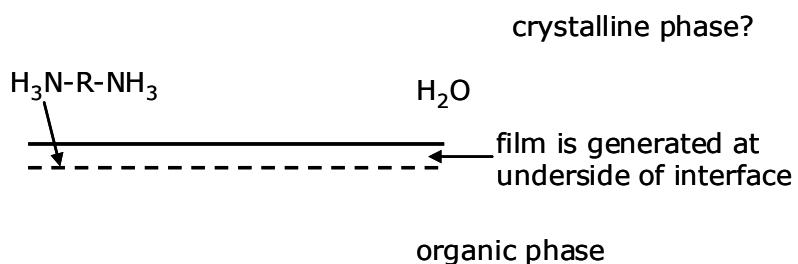
Nonreactive bases:



Avoid bases with HO^- (e.g. NaOH)
Because they can react with acid Cl groups:



-generally true that diamine has higher diffusion rate in organic phase than diacid chloride in H_2O phase



\rightarrow organic solvent \Rightarrow precipitant
must precipitate only high MW polymer

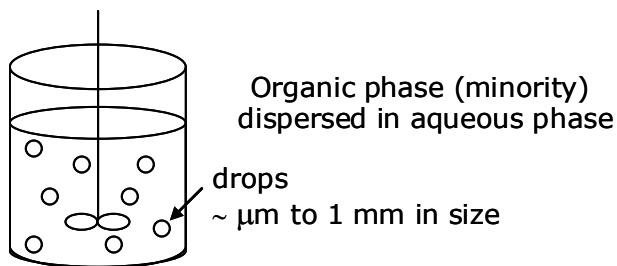
Advantages:

- No need for heavy refrigeration or cooling
(have very little T-increase, phases absorb exotherm)
- Get high MW without perfect conversions or stoichiometry
rate of withdrawal affects MW
when rate \sim formation of chain formation
- Rates of withdrawal, organic solvent choice
- No high- η medium
- Polymer is readily separated from solvent and unreacted monomers

Products made this way:

- aliphatic polyamides
- aromatic polyamides
- polycarbonates
- polysulfides

Stirred Interfacial

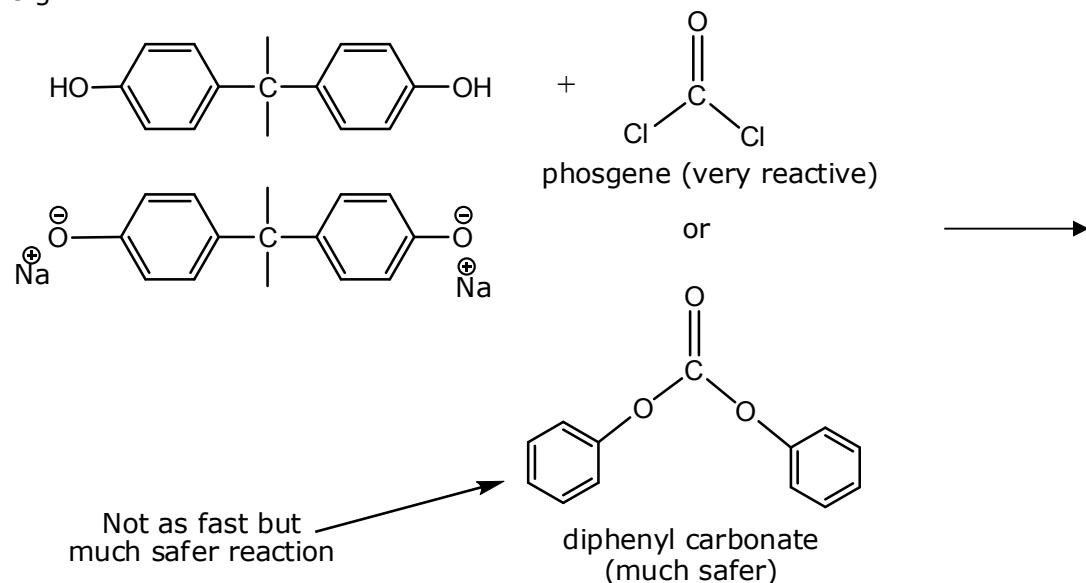


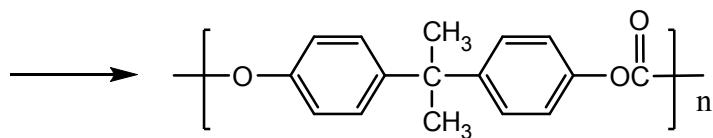
- slow stir rate → generate bubble encapsulating products
- fast stir rate → continuous removal of polymer from droplet
- (shear) → fine particles of polymer
shear can remove polymer film
→ fresh interface
ex. Carbon-less carbon epoxy

Polycarbonates:



e.g.





formed via stirred interfacial process

- high $T_g \sim 150^\circ\text{C}$
- non-crystalline (bulky CH_3 groups to prevent crystalline phase the aromatic groups would try to form)
⇒ fully amorphous → optical clarity
- tough material
- application: CDs, optical lenses, glasses, windshields